



MefHySto

Metrology for Advanced
Hydrogen Storage Solutions



UNIVERSIDADE DA CORUÑA



WP3 : Metrology for Hydrogen Quality from Electrical Energy Storage (HEES) by Hydrogen Back Conversion (Gas-to-Power)

WP leader: CEA
WP partners: NPL, UDC, BAM

Mefhysto Workshop, Berlin, July 3rd - 5th 2023



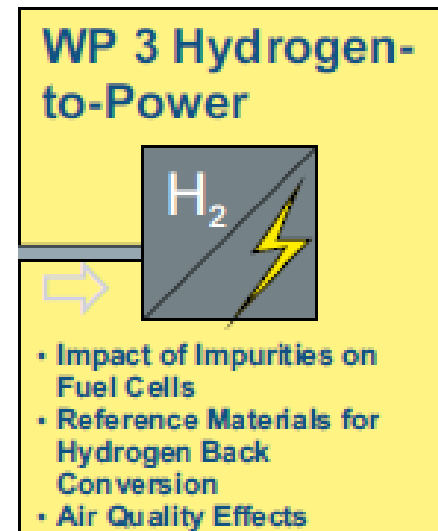
The EMPIR initiative is co-funded by the European Union's Horizon 2020 research and innovation programme and the EMPIR Participating States

• Objectives

- Investigate the sustainability and reliability of FC, whose performance is affected by **impurities in hydrogen and air**
- **Quantify their impact** on PEMFC performances and durability at PEMFC single cell and stack levels
- **Provide data for recommendations** for **air quality sensors** needed for monitoring FC systems;
- **Demonstrate the methodology of contaminant measurements** on a whole hydrogen chain / **Identify contaminants on Hydrogen platforms**

• WP3 is divided into 4 tasks

- Task 3.1 : General literature review, definition and preparation of gas reference mixtures
- Task 3.2: Evaluation and quantification of the impact of relevant contaminants in H₂ supplies for PEM FC for short-term and long-term operation.
- Task 3.3: Evaluation and quantification of the impact of relevant contaminants in Air supplies for PEM FC for short-term and long-term operation.
- Task 3.4: Validation of a metrological chain for gas analysis using a complete demonstration H₂ platform.



• Definition of the H₂ mixtures for PEMFC

- Gas compositions based on:
 - ISO 14687-2 compounds in H₂ such as NH₃, H₂S, CO, new impurities and possible combinations between these contaminants.
 - Other species may be considered based on Mefhysto WP1/WP4/WP5, literature, and related projects HYCORA, HYDRAITE, MetroHyve 1 and 2, Hydrogen.
- “ISO 14687 – like H₂” : Prepared at NPL with relevant contaminants
- Mixtures ready to be used at CEA and NPL for PEMFC testing

| Impurity | ISO 14687:2019 Grade D Limits \\ μmol mol ⁻¹ |
|--|---|
| Water | < 5 |
| Total Hydrocarbons (except Methane) | < 2 |
| Methane | < 100 |
| Oxygen | < 5 |
| Helium | < 300 |
| Nitrogen | < 300 |
| Argon | < 300 |
| Carbon Dioxide | < 2 |
| Carbon Monoxide | < 0.2 |
| Total Sulphur | < 0.004 |
| Formaldehyde | < 0.2 |
| Formic Acid | < 0.2 |
| Ammonia | < 0.1 |
| Halogenated Compounds | < 0.05 |

• Definition of the Air mixtures for PEMFC

| Contaminants | Min conc. tested | Critical value identified in literature (ppb) | Values considered in MEFHYSTO (ppb) |
|-----------------|------------------|---|--|
| NO | 100-300 | 150 | 100 |
| NO ₂ | 100-300 | 150 | 0 (No NO + NO ₂ mixture available) |
| NH ₃ | 200-1000 | 200 | 100 |
| Toluene | 50-100 | 30 | 5 |
| SO ₂ | 10-100 | 10 | 10 |

At CEA : 6 gas bottles available to be diluted in the synthetic air supply

| Gas | Low concentration in N ₂ matrix | High concentration in N ₂ matrix |
|-----------------|--|---|
| Mixture | SO ₂ 5 ppm + 100 ppm NO | SO ₂ 50 ppm + 100 ppm NO |
| Toluene | 5 ppm | 0.5 ppm |
| NH ₃ | 10 ppm | 100 ppm |

Possibility to check also periodic peak effects with x10 high concentrations

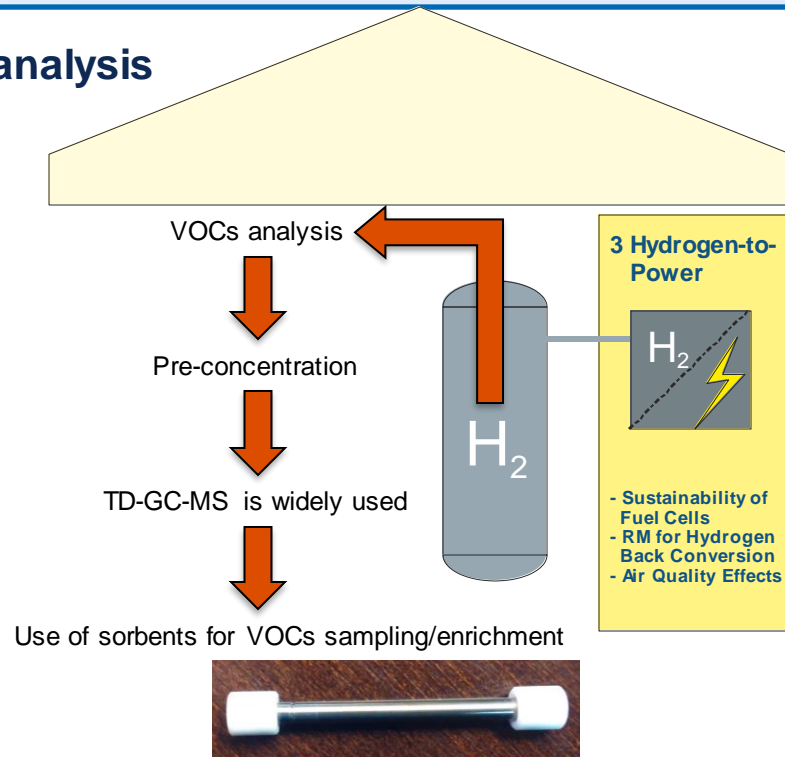
- Misz et al., Sensitivity analyses on the Impact Of Air Contaminants On Automotive Fuel Cells, *FUEL CELLS* 16 (2016), No. 4, 444 – 462.
- Talke, A. et al., Influence of Urban Air on Proton Exchange Membrane Fuel Cell Vehicles - Long Term Effects of Air Contaminants in an Authentic Driving Cycle. *J. Power Sources* 2018, 400, 556–565.
- Schmid et al., Effects of Impurities in the Cathode Airflow on PEM Fuel Cell stacks, *Ext. Abstract A0205, EFCF2021*
- Misz, Effects, Damage Characteristics and Recovery Potential of Traffic-induced Nitric Oxide Emissions in PEM Fuel Cells under Variable Operating Conditions, *FuelCells*, 18 (2018), N°5, 594–601

• Work on the methodology for air sampling and air analysis

Key considerations

- Stability of analytes during sampling, storage and desorption
- Hydrophobicity (moisture can affect adsorption and analysis for some sorbents)
- Artifacts/blank peaks
- Breakthrough volume (limits flow rate and volume that can be sampled)
- Boiling point determines the **sorbent strength** needed

- Strong enough to retain the analytes and weak enough to efficiently release them
- For mixtures with different volatilities a multi-bed sorbents tube can be used
- Weakest sorbent must be first in sampling (to avoid irreversible adsorption of less volatile analytes on the stronger sorbents) and last in desorption

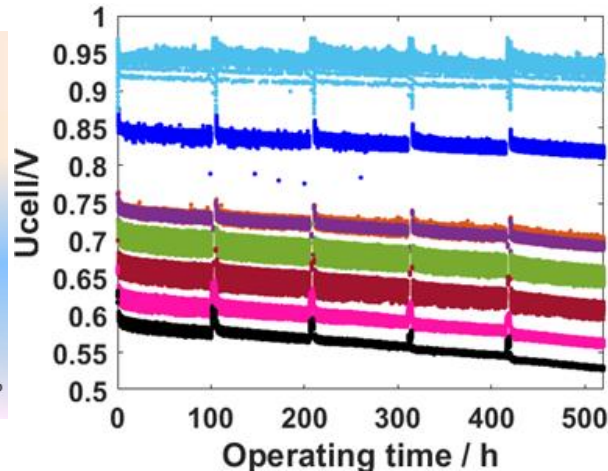
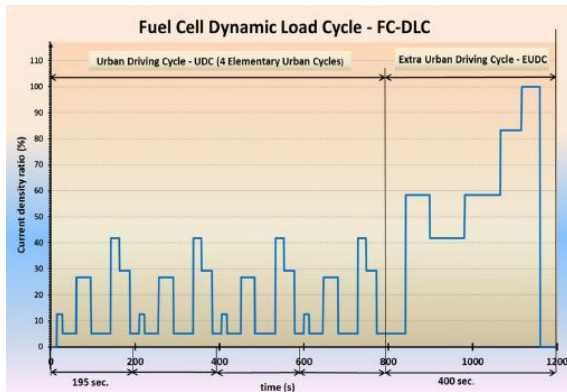


45 halogenated VOCs + qualitative screening for identification of other ones to identify/quantify relevant air contaminants for PEMFC

Impact of contaminants in H₂ and air supplies for PEMFC for short-term and long-term operation

- **Strategy used in the WP for both H₂ and Air:**

- Impact of contaminants studied at 2 main levels :
 - Small single cell under realistic operating conditions : durability study (500-1000h)
 - Short-stack (1 kW) under realistic operating conditions : protocols and short-term performances



25 cm² Single Cell voltage evolution during reference durability tests for 500 h using FC-DLC in 25 cm² single cell

Reference performance and durability data using “pure” reference gases

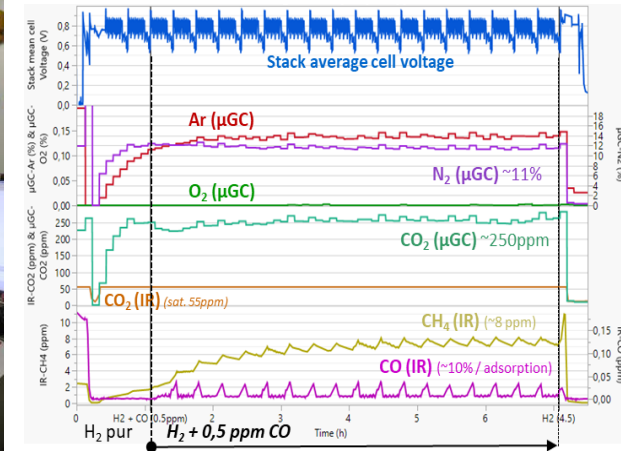
H₂ 6.0 and Synthetic Air

Tests with contaminants planned Q3/Q4 2023 at CEA and NPL

Impact of contaminants in H₂ supplies for PEMFC for short-term and long-term operation

- **Study at short-stack level (~ 1 kW)**
 - **Impact of contaminants on the real-size cell operation** with special attention paid to the **combination of pollutants** and possible decontamination processes
 - **Evaluation of the efficiency** of existing testing protocols available or existing specific **operating conditions for depollution** based on the current density distribution as well as the cell voltage evolution monitoring.
 - **Determination of the reversible/irreversible pollution mechanisms** and their respective impact on both FC performances and degradations.

Stack Test Bench coupled with H₂ gas analysis



Tests planned Q3/Q4 2023
Poster about HYDRAITE results
available during the WS



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Thank you for your attention !



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New metrology for Hydrogen Quality from Power-to-Hydrogen and from Electrical Energy Storage (HEES) by Hydrogen Back Conversion (Gas-to-Power)

Paul Carroll
(National Physical Laboratory, London, UK)

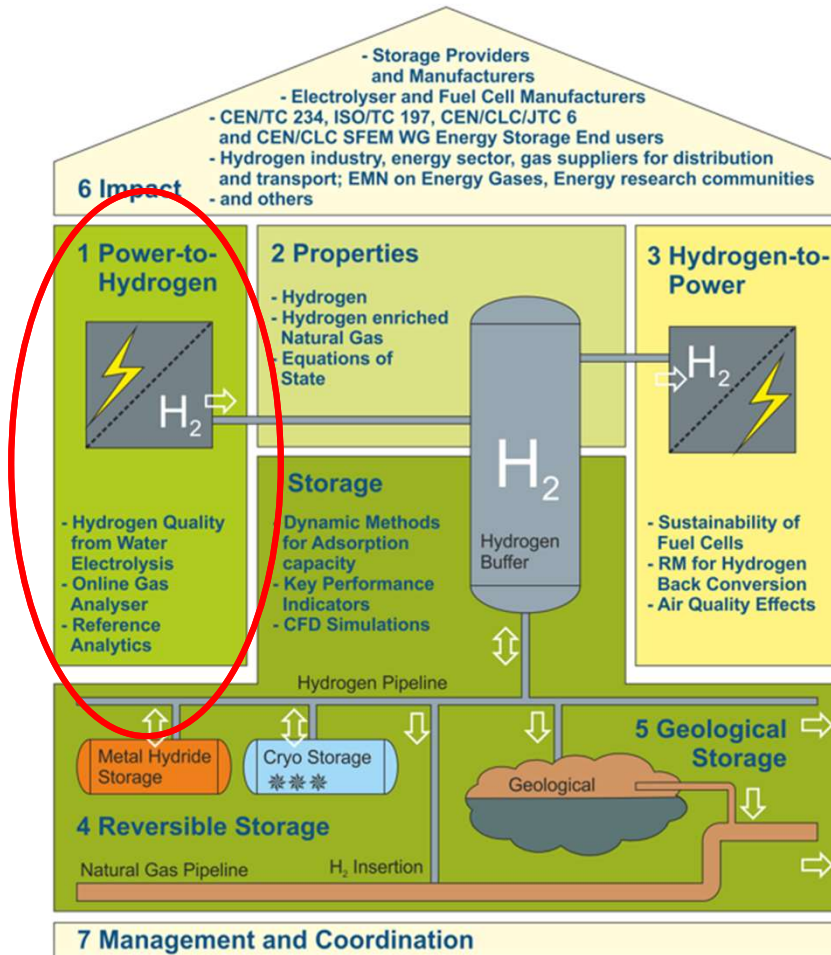


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Session Overview

| | | |
|-------------|---|---|
| 16:00–16:10 | New metrology for Hydrogen Quality from Power-to-Hydrogen and from Electrical Energy Storage (HEES) by Hydrogen Back Conversion (Gas-to-Power) | <u>Paul Carroll</u> (National Physical Laboratory, London, UK) |
| 16:10–16:20 | Assuring Safety and Quality of Hydrogen production | <u>Stephan Zuijendorp</u> , Global Sales, Process Sensing Technologies, Ely, United Kingdom |
| 16:20–16:30 | Metrology for Hydrogen Vehicles2 – Overview of project achievements | <u>Thomas Baquart</u> , (National Physical Laboratory, London, UK) |
| 16:30–17:30 | Workshop (Quality from Water Electrolysis, Online Gas Analysis, Reference Analytics, Impact of Impurities on Fuel Cells, Reference Materials, Air Quality Effects) | Experts from the MefHySto consortium |
| 16:30 | Introduction to workshop | <u>Paul Carroll</u> , (National Physical Laboratory, London, UK) |
| 16:30-16:50 | Topic 1: Electrolysers / effects of impurities on fuel cells. 10 minute presentation followed by panel discussion. | <u>Jonathan Goh</u> , (National Physical Laboratory, London, UK) and <u>Fabrice Micoud</u> (Commissariat à l'Énergie Atomique et aux Énergies Alternatives, Grenoble, France) |
| 16:50-17:10 | Topic 2: Online Gas Analysis for quality measurement / reference analytics. 10 minute presentation followed by panel discussion. | <u>Paul Carroll</u> , (National Physical Laboratory, London, UK) |
| 17:10-17:30 | Topic 3: Reference material production / reference analytics. 10 minute presentation followed by panel discussion. | <u>Ziyin Chen</u> , <u>Thomas Baquart</u> , (National Physical Laboratory, London, UK), <u>Michael Maiwald</u> , <u>Dirk Tuma</u> , BAM, Berlin, Germany |

WP1: New Metrology for Hydrogen Quality from Power-to-Hydrogen



- Internal funded partners



- External funded partners



- Better understanding of the parameters influencing water electrolysis under process conditions.
- Detailed investigations on energy processes and load conditions are still lacking, including short-term peak energy loads of up to 200 %. These must be handled safely in order to prevent quality problems or damage to fuel cells (FC) and peripheral equipment.
- Go beyond the state of the art by investigating the quality of hydrogen produced from PEM water electrolysis during rapidly imposed transient use periods.
- This will be done with online gas analysers used for measuring key impurities such as water vapour and oxygen calibrated against standards developed by project partners.

WP1: New Metrology for Hydrogen Quality from Power-to-Hydrogen

Task 1.1: New metrology for realisation and measurement of key impurities in hydrogen, with fast response times

develop new metrology for the measurement of key impurities in hydrogen (including water vapour and oxygen) produced from PEM water electrolyzers with fast response times of a few or tens of seconds (i.e. the timescale of surges in electricity demand and supply).

Task 1.2 Testing and validation of instruments for measuring key impurities in hydrogen

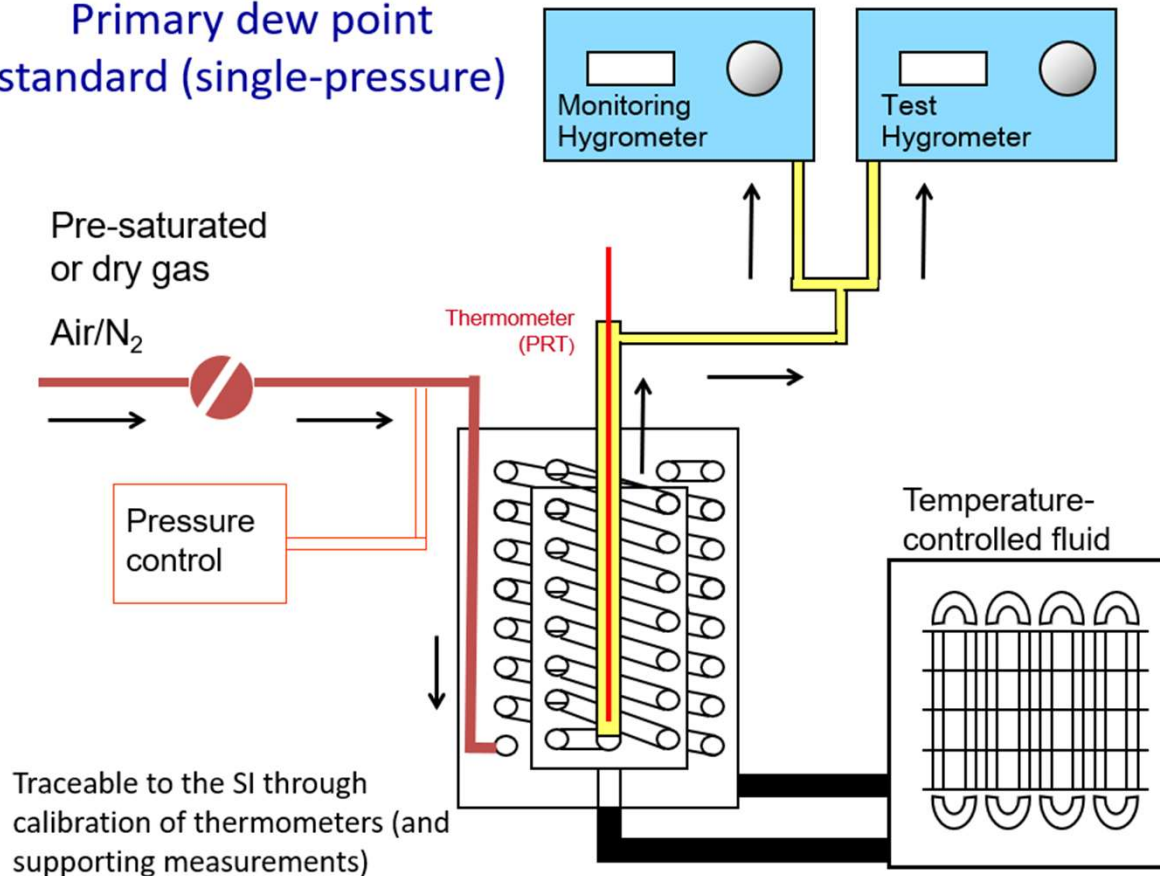
validate the performance of instruments for measuring key impurities (principally water vapour and oxygen) in hydrogen including the spectroscopic method developed and validated in Task 1.1 and existing online gas analyser instruments with suitably fast response times.

Task 1.3: Trials of rapid response analysis of key contaminants of hydrogen from electrolysis

demonstrate measurements of contaminants in-situ in hydrogen generated from electrolysis. This will be done by trialling the PEM water electrolyser test system developed in Task 1.1 and the other instruments for in-process measurement of contaminants in hydrogen characterised in Task 1.2, as well as a micro GC. Results presented in workshop later today.

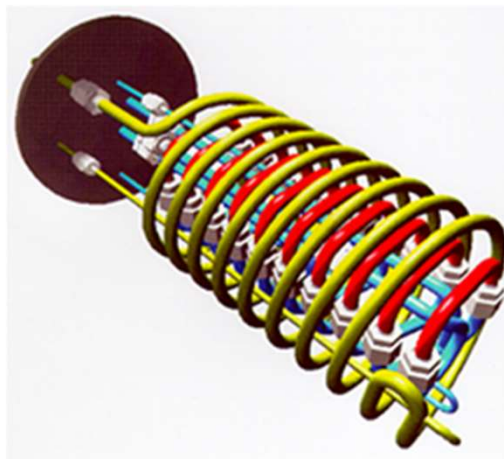
NPL Dew-point hygrometer calibration standard

Primary dew point standard (single-pressure)

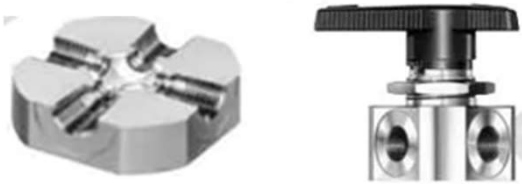


NPL Multi-gas, Multi-pressure primary standard humidity generator

- Moderately inert gases (e.g hydrogen, methane, argon)
- Pressures up to 3 MPa (30 bar)
- Dew/frost point range -60 °C to +15 °C ($k = 2$ expanded unc. = 0.12 °C)
- Hybrid generator: calibration in single pressure dew-point mode
- Ability to mix wet & dry gases using array of mass flow controllers

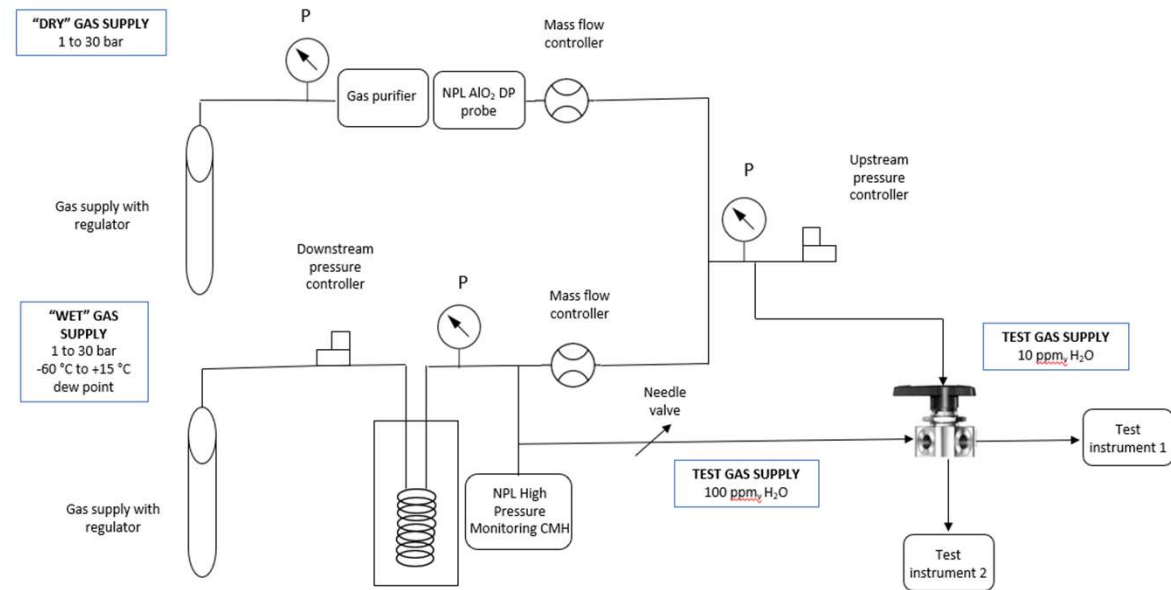


NPL humidity response time testing facility

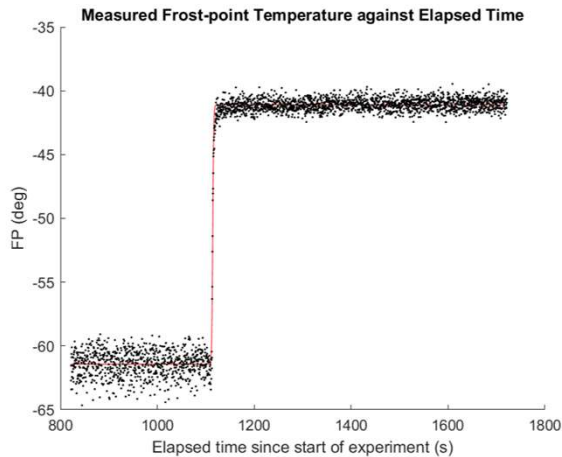


Source: Swagelok

- 4-way valve used to make fast step changes in water vapour in conjunction with NPL Multi-gas, Multi-pressure Primary Standard Humidity Generator. Volume of path lengths between valve and test instruments kept as small as possible.
- Dilution of “wet” gas with “dry” gas using MFC flow-mixing approach means two dynamic sources of different humidities can be simultaneously generated with a range of water content values accessible.



NPL humidity response time testing analysis

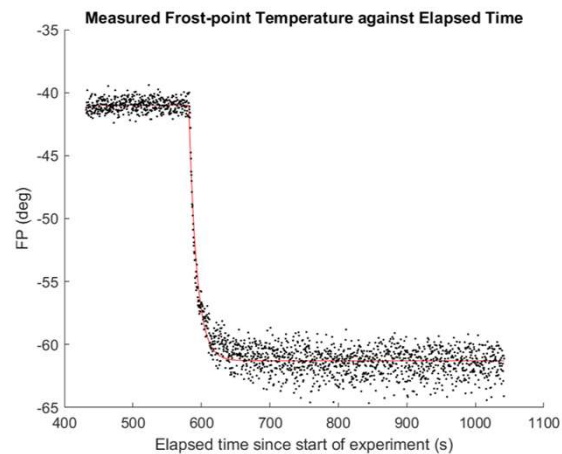


Functions written by NPL Data Science group in MATLAB perform fitting to measured data and estimate t_{90} rising and falling values.

Sigmoid function fit analysis for rising series,

Exponential decay function for falling series.

Uncertainty estimate in calculated response time estimate due to scatter and curve fitting is also evaluated.

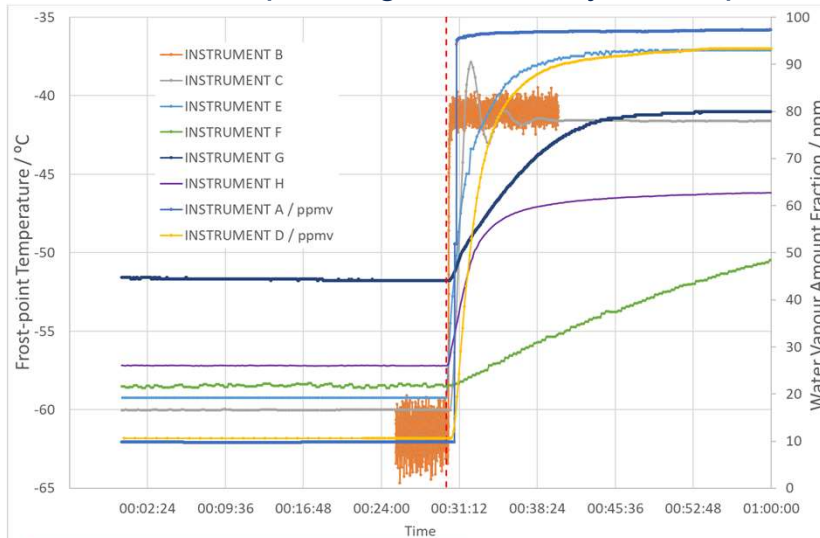


Eight instruments loaned from collaborators tested for pressure and background gas measurement error dependency as well as response time analysis. Some example results and their implications to quality measurements discussed in workshop later.

Sensing principles include: chilled-mirror hygrometer, metal-oxide dew point probe, water vapour spectrometer, surface acoustic wave, fibre optic method sensing principle, electrolytic P_2O_5 .

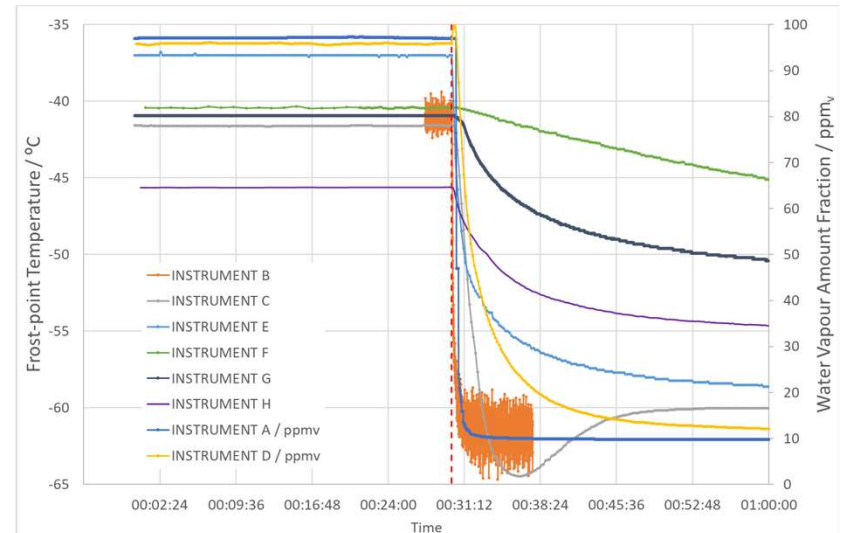
Task 1.2: Testing and validation of instruments for measuring key impurities in hydrogen

- NPL Humidity and NPL Gas Metrology:** Using input from (A1.2.1), (A1.2.2) and the NPL primary (dynamic) humidity generation facilities, NPL will assess the response time (performance) of online gas analysers and sensors of water vapour and oxygen. NPL will use the step change test facility developed in A1.1.2 for the assessment. (A1.2.4)



| Instrument | t_{90} response time / s |
|--------------|----------------------------|
| INSTRUMENT A | 19.30 |
| INSTRUMENT B | 2.14 |
| INSTRUMENT C | 26.83 |
| INSTRUMENT D | 164.84 |
| INSTRUMENT E | 306.13 |
| INSTRUMENT F | 6872.48 |
| INSTRUMENT G | 786.62 |
| INSTRUMENT H | 402.72 |

t_{90} for INSTRUMENT F = 115 minutes



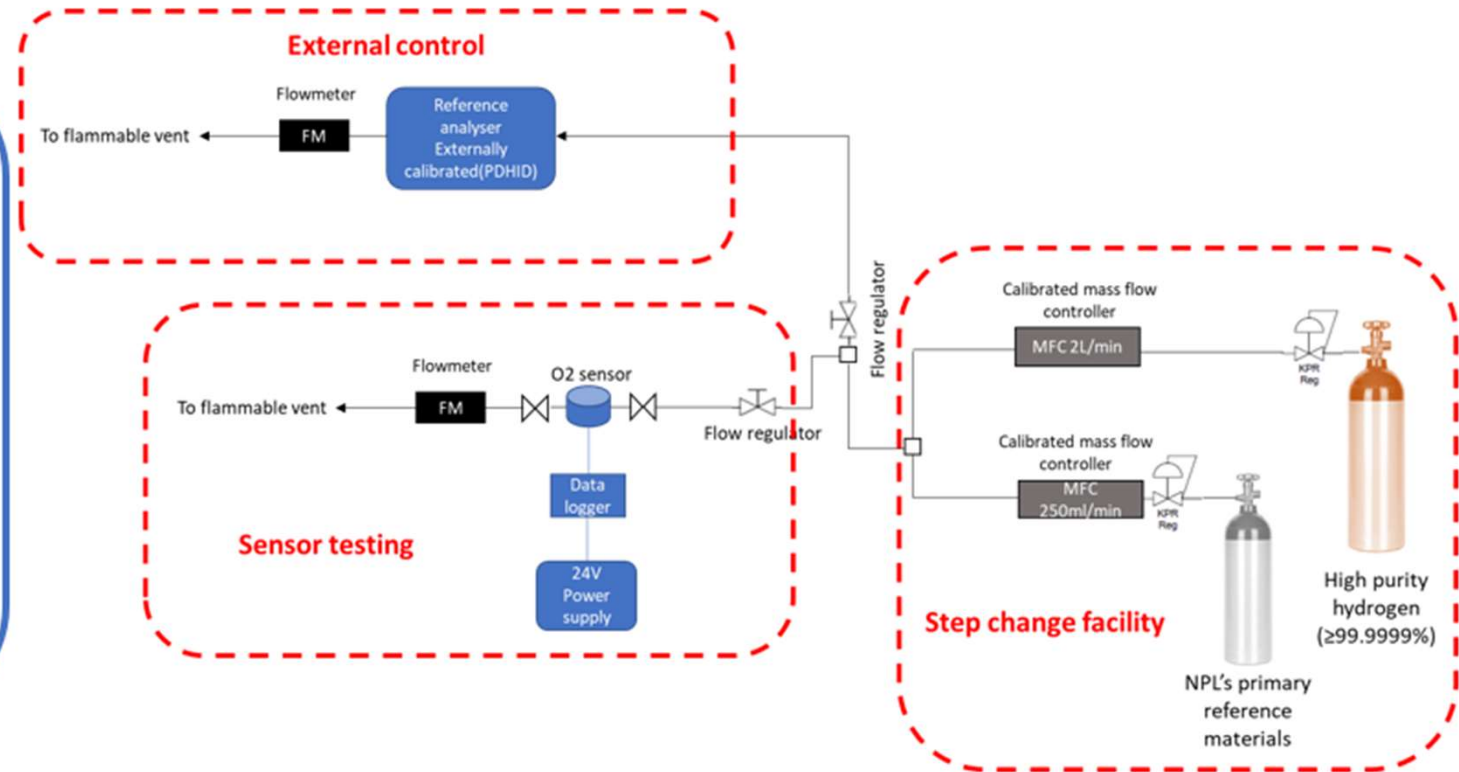
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| Instrument | t_{90} response time / s |
|--------------|----------------------------|
| INSTRUMENT A | 28.32 |
| INSTRUMENT B | 26.28 |
| INSTRUMENT C | 117.9 |
| INSTRUMENT D | 417.8 |
| INSTRUMENT E | 449.5 |
| INSTRUMENT F | 16822 |
| INSTRUMENT G | 3452 |
| INSTRUMENT H | 2580 |

t_{90} for INSTRUMENT F = 280 minutes

Task 1.1 – (A1.1.2) NPL O₂ sensor response time testing set up

- NPL developed a bespoke step change facility for sensors validation
 - Rapid change of amount fraction;
 - Traceability to NPL's PRM;
 - Flexible flow rate;
 - External validation of amount fraction via a parallel line to NPL calibrated gas analyser.



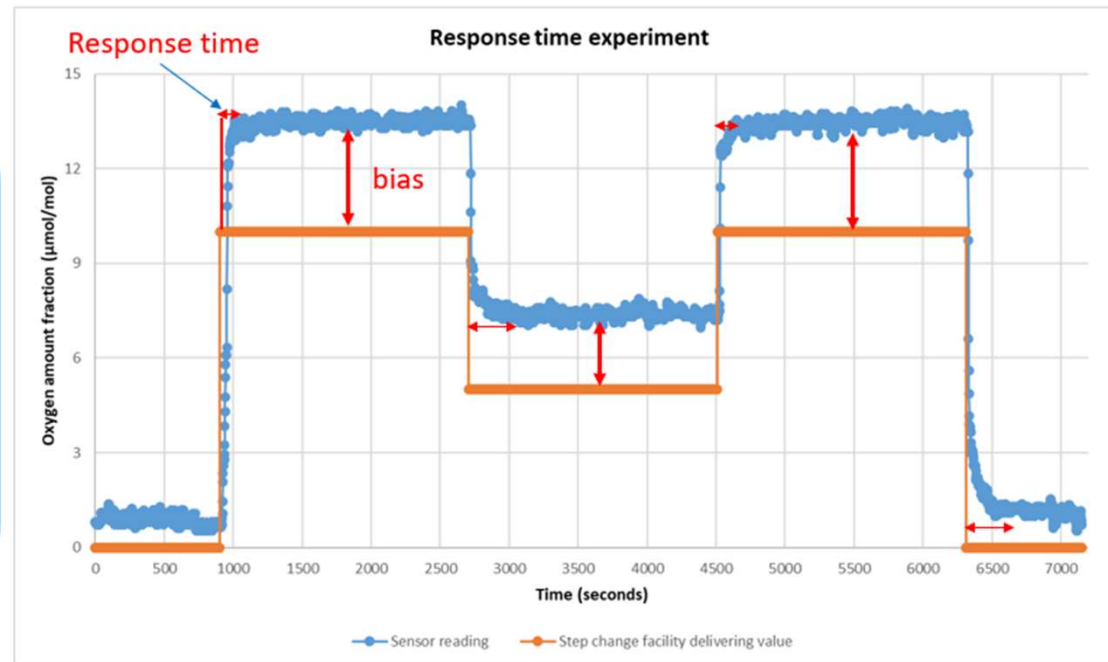
Achievements: compatible with most contaminants in H₂ (i.e., O₂ from 0.5 to 20 μmol/mol); fast response (< 20 seconds)

Task 1.1 – (A1.1.2) NPL O₂ sensor response time testing set up

Example of experimental results

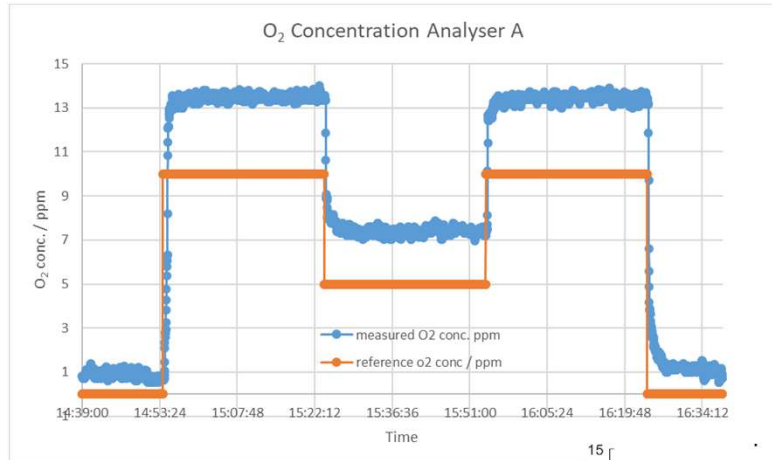
Experimental conditions:

- Oxygen sensor A
- Amount fraction 0, 5, 10 $\mu\text{mol/mol}$ oxygen in hydrogen
- Response time: < 5 sec from NPL Step change facility
- Pressure: 1.04 bar
- Flow rate: 0.44 L/min
- Temperature: 20 °C

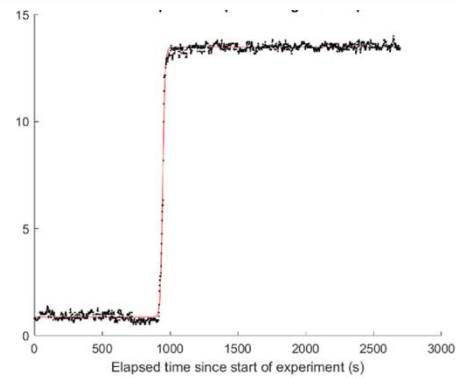


- The sensor A responded rapidly to the change of oxygen amount fraction in hydrogen gas
- Significant bias observed (nearly 25 to 30%) between actual reading from sensor and theoretical value
- Impact: (+) fast response from sensor achieved / (-) inaccurate information to end users
- Further modifications/improvements for sensors: improve trueness.

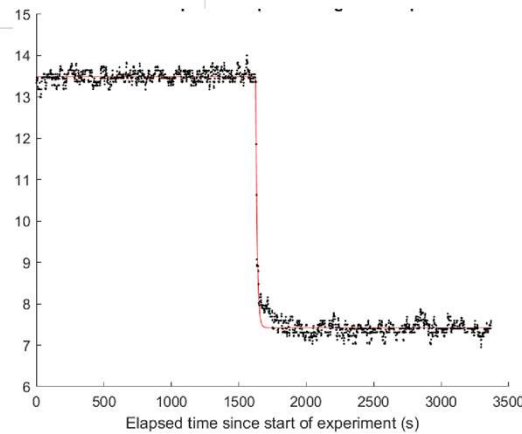
Task 1.1 – (A1.1.2) NPL O₂ sensor response time testing results



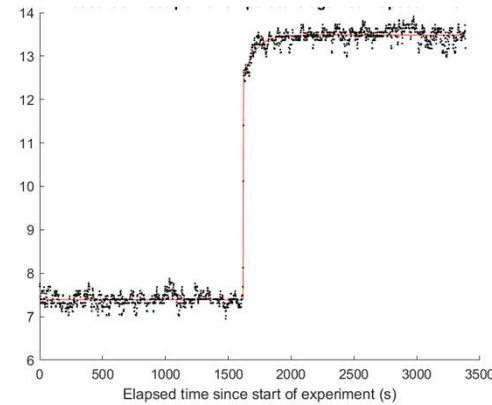
| Step change O ₂ / μmol mol ⁻¹ | Time / s |
|---|----------|
| 0 – 10 rising | 73 |
| 5 – 10 rising | 29 |
| 10 – 0 falling | 76 |
| 10 – 5 falling | 35 |



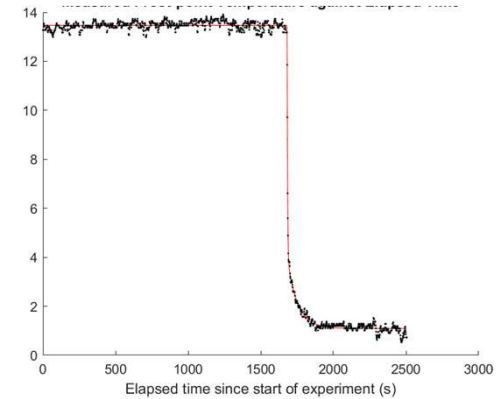
0 – 10 μmol mol⁻¹



10 – 5 μmol mol⁻¹



5 – 10 μmol mol⁻¹



10 – 0 μmol mol⁻¹

Task 1.1 - A1.1.1 Progress month 22

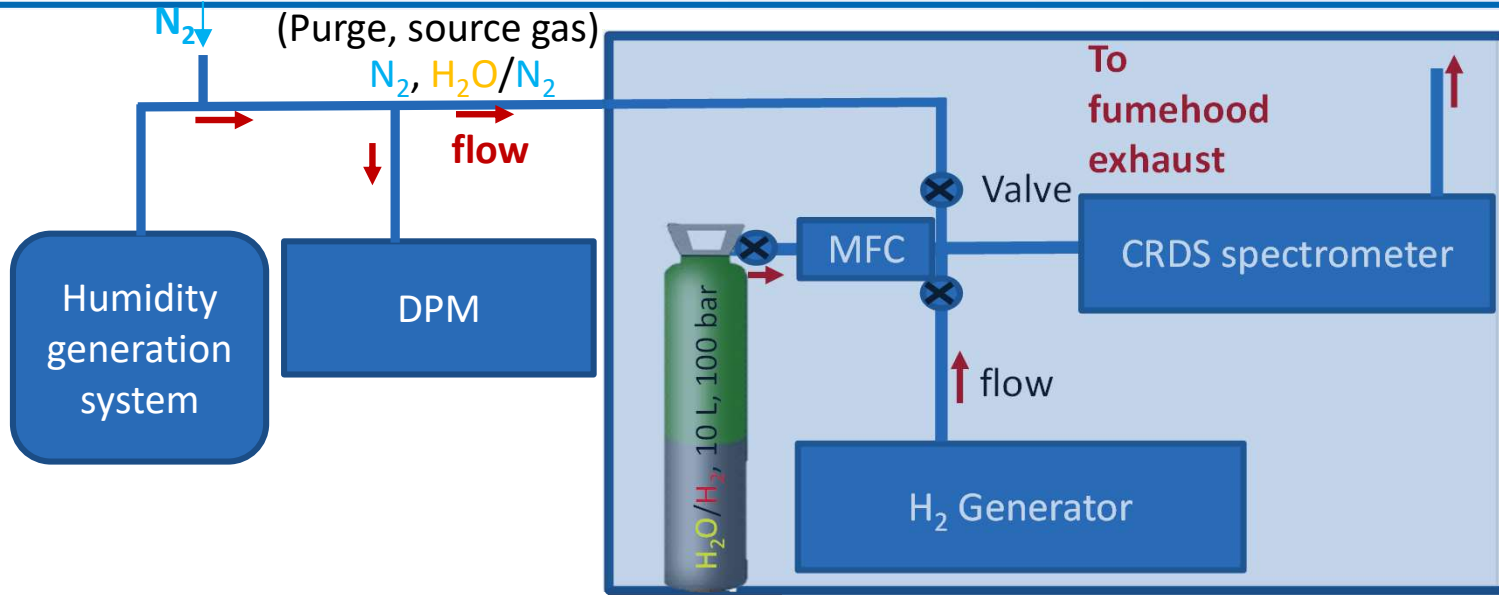


will develop a metrologically compatible laser-spectrometric measurement method for fast H₂O impurity measurements in H₂.
(A1.1.1)

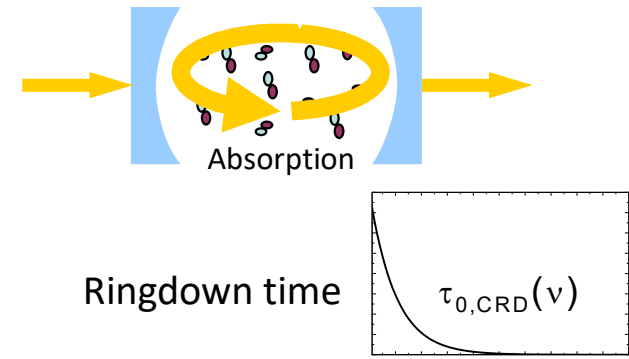


- **PTB:**
- Tiger Optics Halo HALO-RP has been selected as a suitable instrument to adapt for the application specificities.
- The measurement principle for this instrument is Cavity Ring-Down Spectroscopy (CRDS). Maximum measurement range 10 ppm H₂O.
- Trial measurements to be made at PTB with nitrogen background gas prior to arrival of water vapour reference cylinders in Hydrogen from **NPL Gas Metrology**.
- Reference cylinders prepared by **NPL Gas Metrology** with 2 $\mu\text{mol mol}^{-1}$, 5 $\mu\text{mol mol}^{-1}$ and 10 $\mu\text{mol mol}^{-1}$ water vapour in hydrogen amount fractions and sent to PTB.
- Mixtures validated against NPL gravimetric standards and NPL humidity standards.

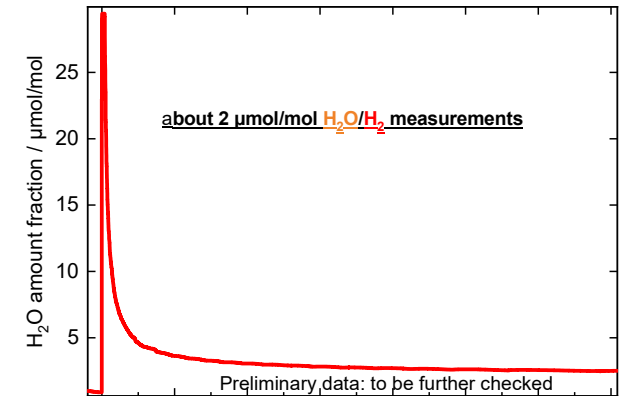
PTB Progress Task 1.2 – (A1.2.6)



Cavity Ringdown spectroscopy (CRDS)



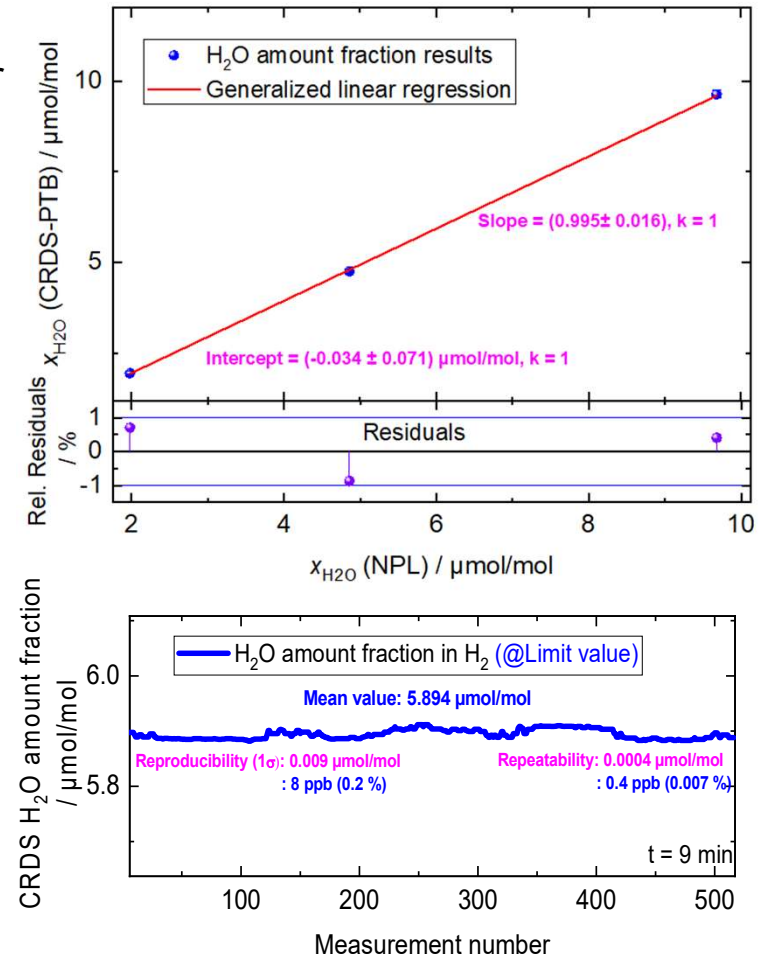
- Measurements have been performed with the mixtures from A1.2.2 (provided by NPL: 2, 5 10 $\mu\text{mol/mol}$ H_2O in H_2).



PTB Progress Task 1.2 – (A1.2.6)

- Measurements are done employing a laser spectrometric method based on **cavity ring down spectroscopy –CRDS** for H₂O impurity measurements in H₂.
- Measurements with H₂O in H₂ mixtures provide by NPL demonstrates a good linearity of the method/instrument.
- At the ISO14687 limit value (5 μmol/mol H₂O in H₂), the reproducibility of the measurements is 0,008 μmol/mol (0.2 %, 1σ, over 9 minutes).

| Contaminant in H ₂ | H ₂ O-Limit in H ₂ (ISO14687) |
|-------------------------------|---|
| H ₂ O | 5 μmol/mol |



Task 1.1 – Establishment of PEM water electrolyser test systems



will establish a PEM water electrolyser test system (single cell) with online impurity measurement at the cathode. (A1.1.3)



will perform single cell testing to study the impact of operating conditions and transient profiles on the cell performances and on the quality of produced hydrogen with online sensor. (A1.1.3)

CEA: PEMWE testing at single cell level test bench specifications

- 25 cm² single setup, Circular active area, Titanium monopolar plates
- Titanium foam as porous layer at the anode
- Gas Pressure : up to 10 bar abs.
- Cell temperature: up to ca. 80°C (external heating) + water supply (0-1000 mL/h) heating.
- Current supply: 0-100 A, Gas flow rates: 41 NI/h for H₂ and 20 NI/h for O₂



Commercial electrolyser Hogen S20 specifications

- 10 cell-stack, Stack current can be controlled by the CEA control-command software
- No internal H₂ purifier, Drying by 2 zeolite units (regenerated with dry H₂ bypass by alternative operation)
- Asymmetrical operation: atmospheric pressure at the anode / 15 bar at the cathode

- Gas analysis for %H₂ in O₂ by catharometer equipment but not really precise (drifts in time due to “wet gas”)
- μ GC available for more precise measurement H₂ in O₂ and O₂ in H₂ but only periodic sampling.
- Gas mixtures were obtained to calibrate sensor in the electrolyser at CEA after it was re-started.





Thank you! Questions?

Paul Carroll, (National Physical Laboratory –NPL, London, UK)
paul.carroll@npl.co.uk



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Online Gas Analysis for hydrogen quality measurement and reference analytics

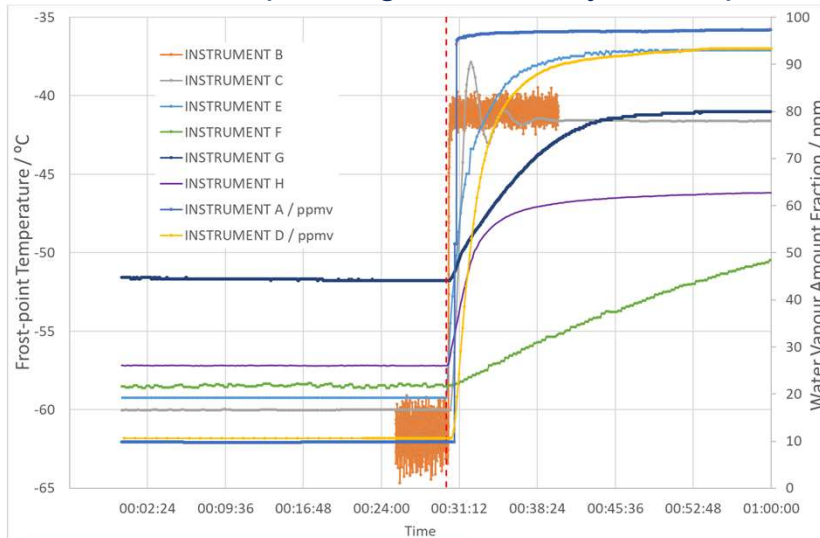
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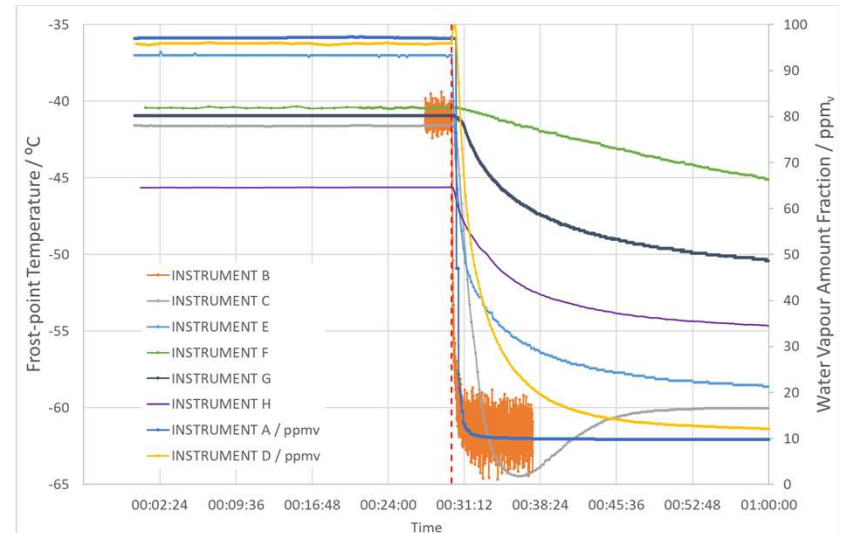
Task 1.2: Testing and validation of instruments for measuring key impurities in hydrogen

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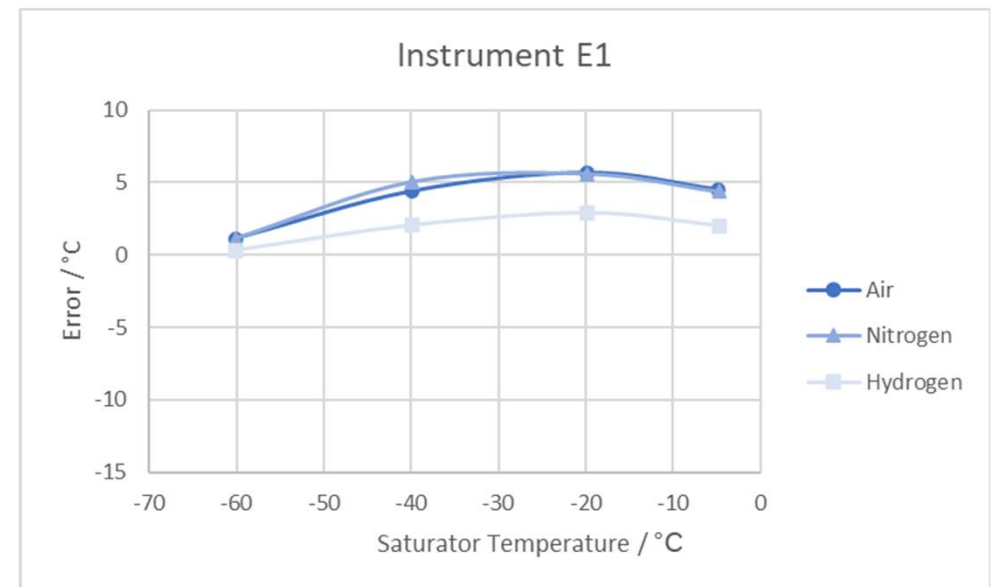
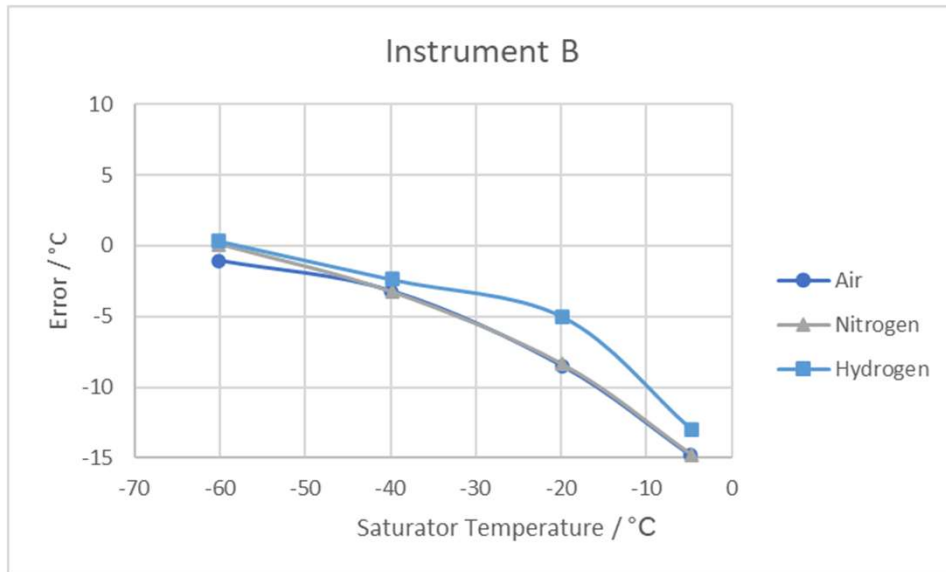
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t_{90} for INSTRUMENT F = 280 minutes

- A slow response to a humidity change from an online monitoring sensor would result in delays to measurements of the true moisture value.
- Process monitoring would be slow to react resulting in potential gas quality implications or wasted energy on needless over-drying.
- **Sensor response:**
 - Rising or falling step change – t_{90} significantly faster for rising changes for all instruments tested
 - Sensing principle
 - Measurement interval of instrument / logging software (ranged from 0.3 s to 10 s)
 - Ambient temperature (NPL can vary this using environmental chambers)
- **System related:**
 - Volume of connecting pipework / housing of sensor
 - Flow-rate of gas to sensor

Task 1.2: Testing and validation of instruments for measuring key impurities in hydrogen

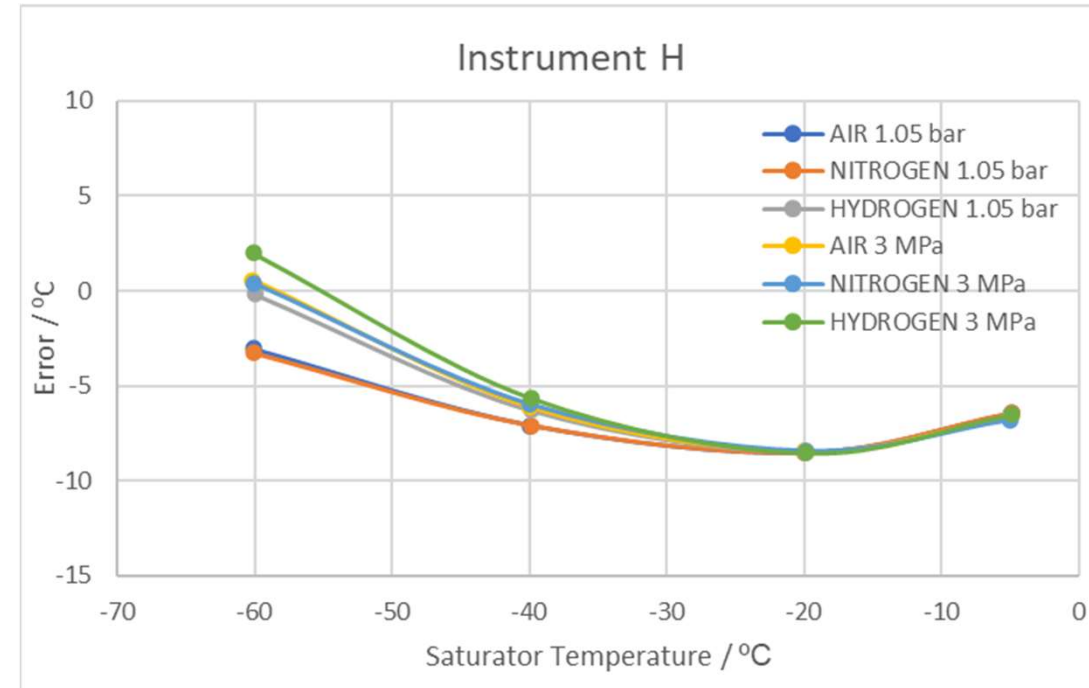
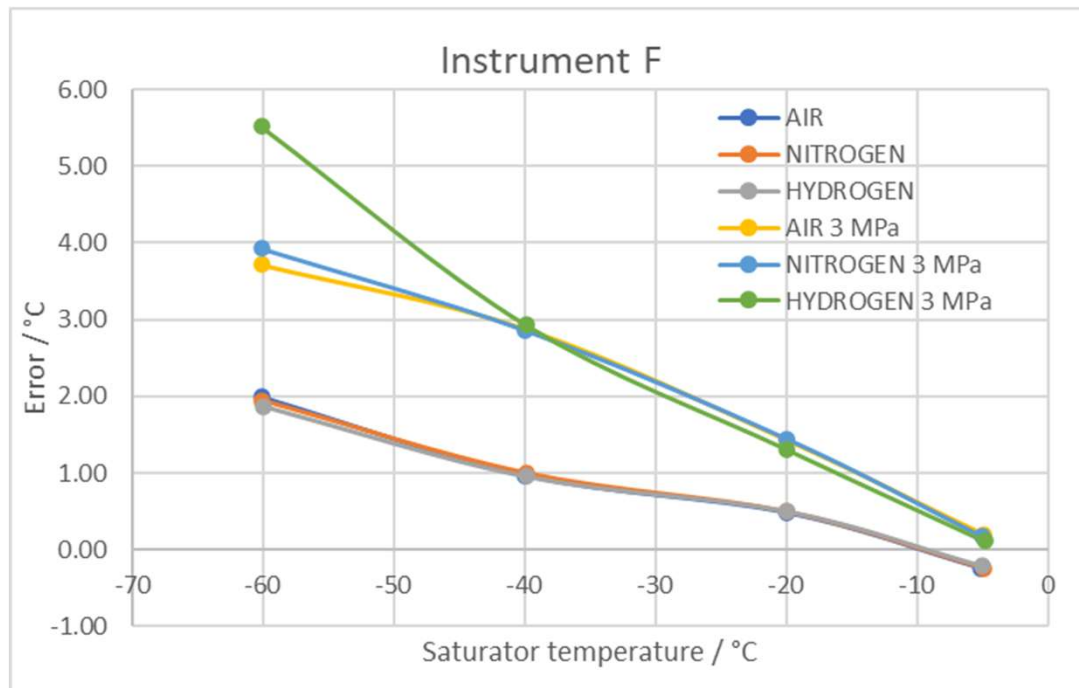
NPL Humidity: will assess at least four commercially available instruments for measuring water vapour, to evaluate influence of pressure and **of hydrogen** as background gas using the gas mixtures and the NPL Multi-gas, Multi-pressure Humidity Generator (A1.2.3)



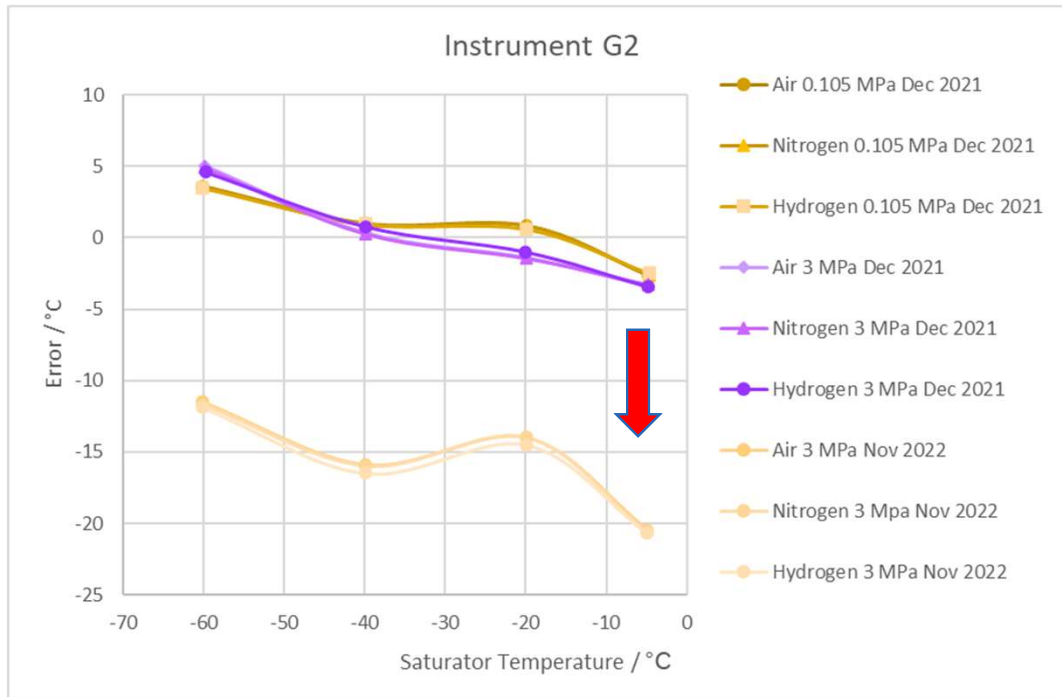
Note: Instruments shown only recommended for use at atmospheric pressure

Task 1.2: Testing and validation of instruments for measuring key impurities in hydrogen

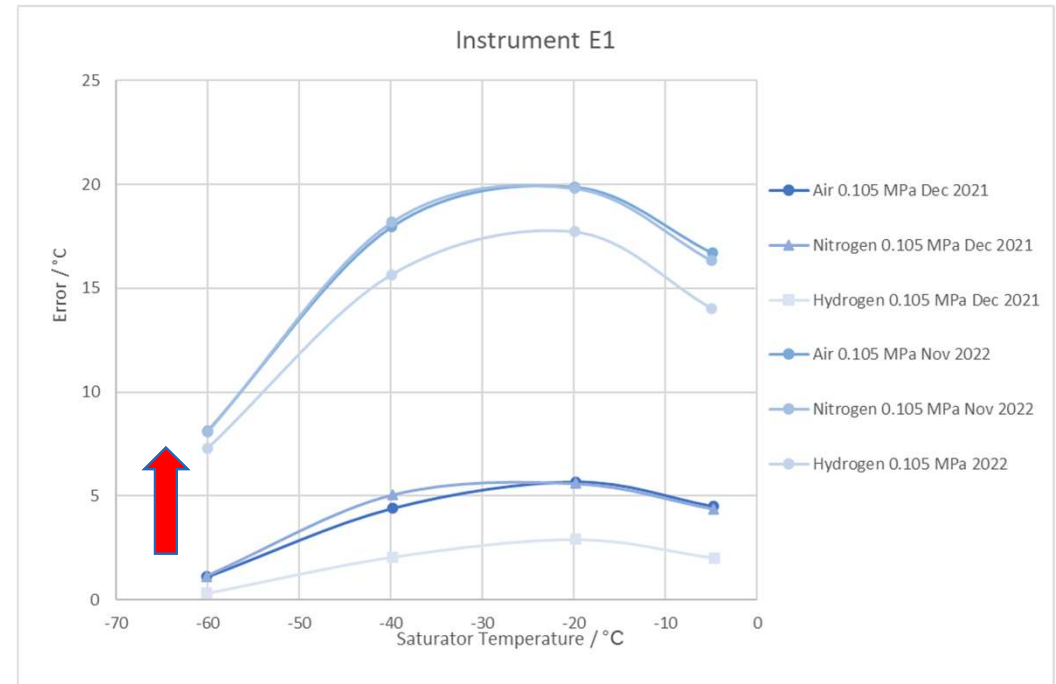
NPL Humidity: will assess at least four commercially available instruments for measuring water vapour, to evaluate influence of **pressure and of hydrogen** as background gas using the gas mixtures and the NPL Multi-gas, Multi-pressure Humidity Generator (A1.2.3)



Example results of instrument long-term drift



Error drift towards under reading



Error drift towards over reading

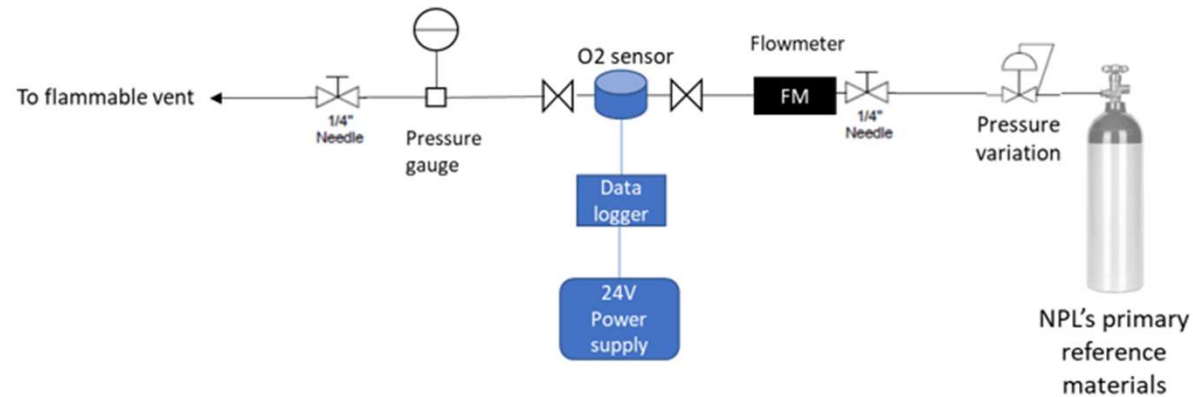
Recommendations when requesting hygrometer calibrations:

- Use a laboratory with ISO 17025 accreditation for humidity calibration in the relevant range
 - Request that the calibration is in the working units of the hygrometer e.g. dewpoint temperature ($^{\circ}\text{C}$) or volume fraction (ppm_v)
 - Request at least three points covering minimum and maximum expected humidity values of the process being monitored
 - If possible, request that calibration is performed in the background gas and the pressure the hygrometer would experience during service
 - Request an “as-found” calibration of the hygrometer at the end of service to assess long-term drift.
-
- *Good Practice Guide: Calibration and use of humidity sensors for hydrogen refuelling station applications:*
 - www.sintef.no/globalassets/projectweb/metrohyve-2/d5-a3.2.2-good-practice-guide-on-calibrating-commercial-humidity-sensors.pdf

Task 1.2: Testing and validation of instruments for measuring key impurities in hydrogen

NPL Gas Metrology: will assess at least two commercially available instruments for measuring oxygen, to evaluate influence of pressure, linearity, (A1.2.3)

NPL experimental setup



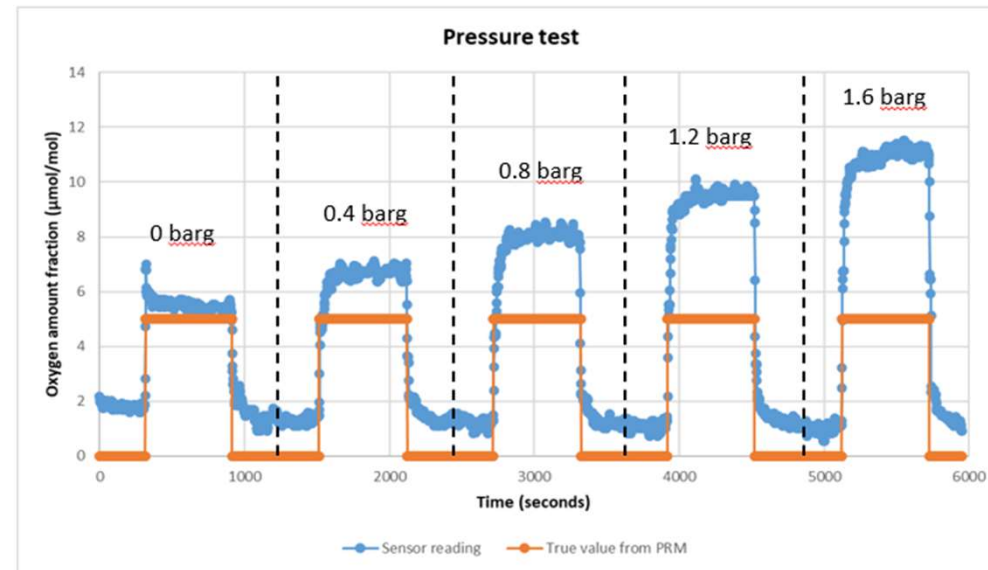
- Current capability: 0 – 20 barg depending on sensor specification
- Experiment test realised from 0-1.6 barg at 5 $\mu\text{mol/mol}$ oxygen in hydrogen on 2 different sensor types

Task 1.2: Testing and validation of instruments for measuring key impurities in hydrogen

NPL Gas Metrology: (A1.2.3)

Experimental results of pressure test which was conducted with a primary reference material (5 ppm O₂ in H₂).

- ✓ The system pressure was increased from atmospheric pressure to 2.6 bar
- ✓ Between each experiment under different pressure, the system was reduced to atmospheric pressure and purged with pure hydrogen to prevent any interference.
- ✓ The flowrate was adjusted to a constant (0.4 L/min)



Note:
Manufacturer's specification states only to be used at atmospheric pressure only !

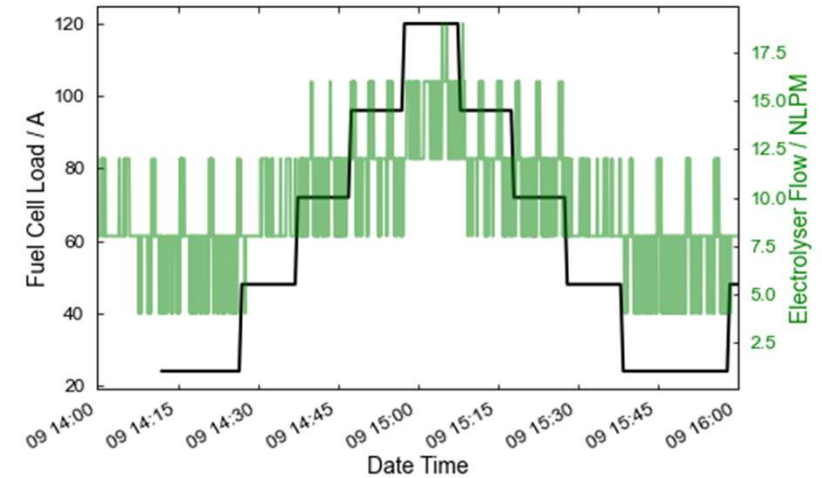
Highlights:

- impact on sensor accuracy observed due to small pressure changes
 - Response x 2 from atmospheric pressure to 2.2 bar
- Other sensors under evaluation – looking for new sensor manufacturer feedback or joint activity

Task 1.3: Trials of rapid response analysis of key contaminants of hydrogen from electrolysis

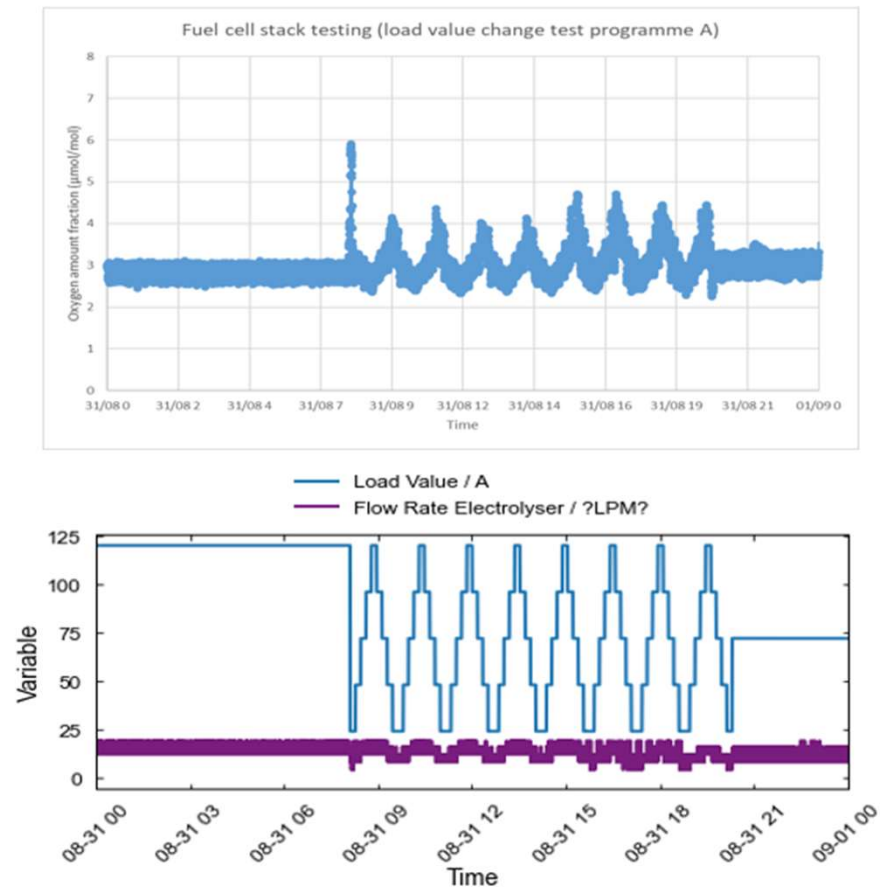
- **(A1.3.1) NPL**, CEA, PTB and DBI will develop protocols for laboratory and field trials of the spectroscopic method (A1.1.1) and validated in A1.2.6, together with the online gas analyser instruments characterised in A1.2.3, A1.2.4 and A1.2.5.

| | | | |
|-------------------|--|-------|--|
| NPL | | | |
| Production | | | |
| Equipment | Hogen S Series 2 Hydrogen Generator S40 | | |
| Max Rate | 1.05 | Nm3/h | |
| Max Pressure | 14 | barg | |
| Purity | 99.9995 | % | |
| | < 5 ppm water (-65 deg C dew point atmospheric pressure) | | |
| | < 2 ppm N2 | | |
| | < 1 ppm O2 | | |



Task 1.3: Trials of rapid response analysis of key contaminants of hydrogen from electrolysis

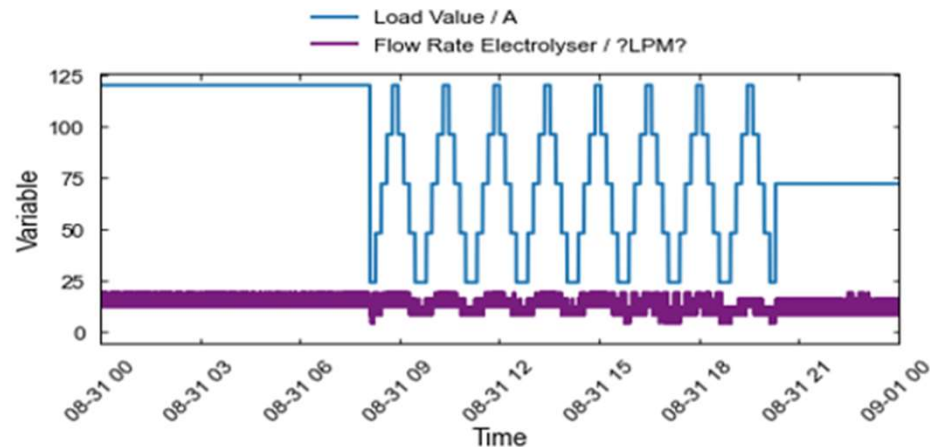
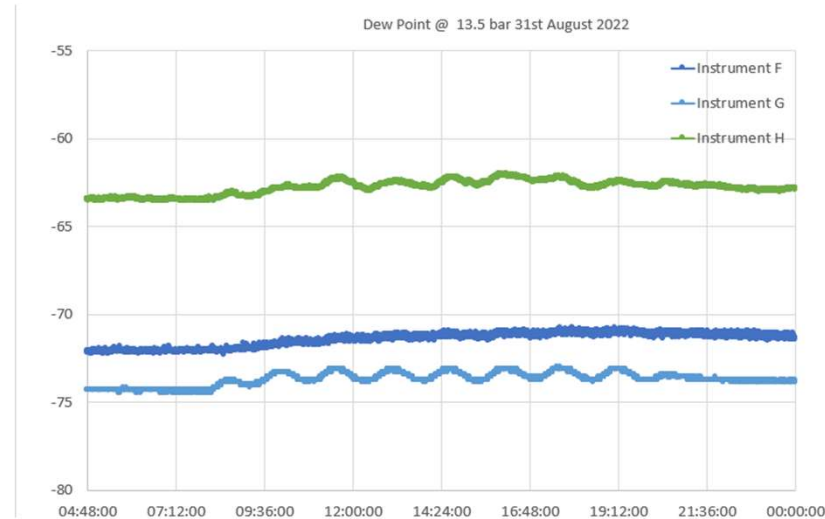
Application of sensor in real life situation: electrolyser



- Lack of rapid response analyser for oxygen at low $\mu\text{mol/mol}$ amount fraction
 - Sensor are good option to monitor such changes for oxygen or water amount fraction
- Sensor response vary with electrolyser load change
 - Real change or Change related to operation parameters of the electrolyser (pressure, temperature, flow rate)?
- Importance to understand the rapid changes of electrolyser parameters in term of hydrogen quality
 - Is the change related to metrological issue or to hydrogen quality change from the system?
- Further works:
 - monitoring all electrolyser gas parameters (pressure, flow variation)
 - correlate the results of the study (i.e., pressure impact accuracy) with real life measurement and conditions

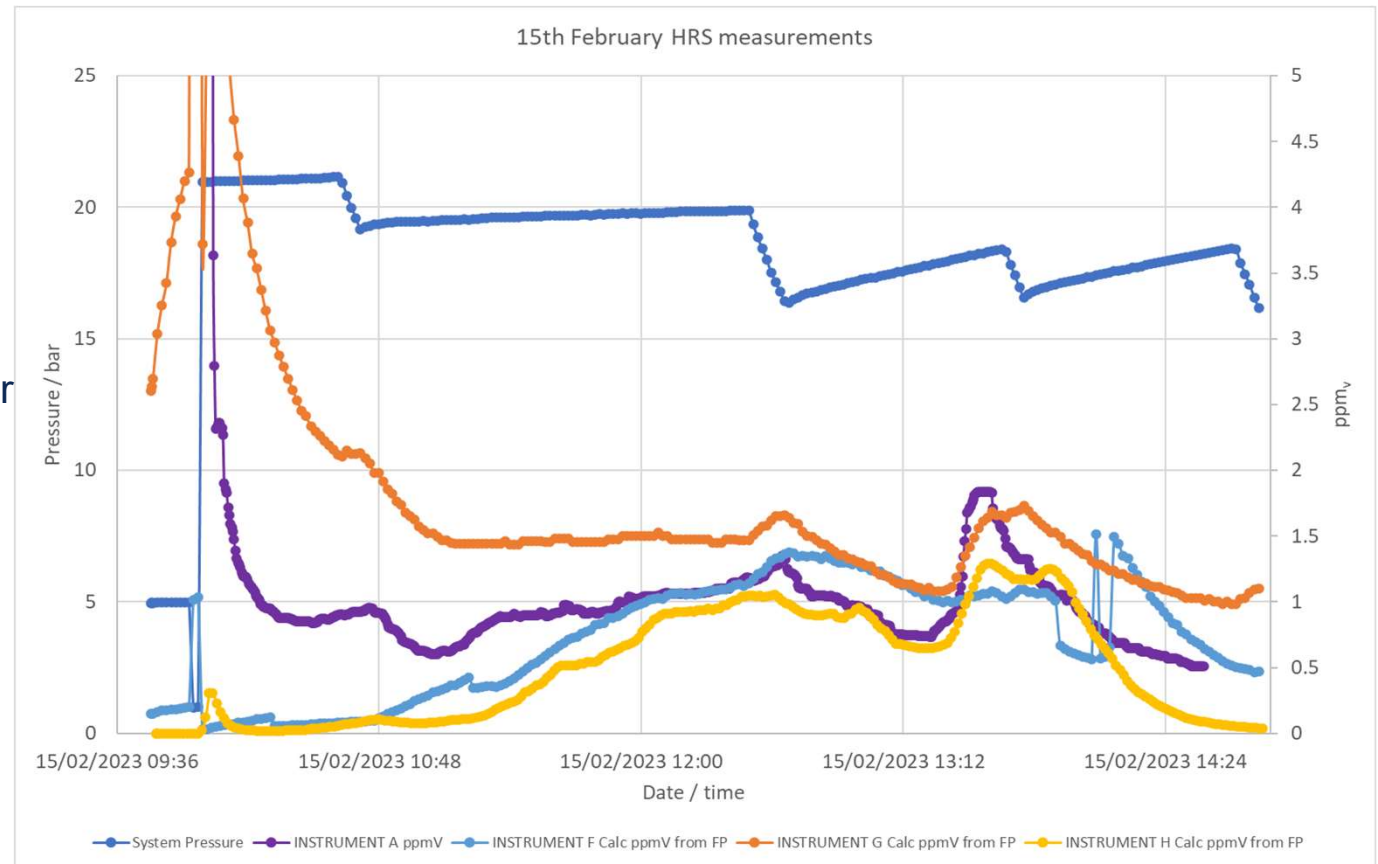
Task 1.3: Trials of rapid response analysis of key contaminants of hydrogen from electrolysis

- Dew-point temperature measurements made of Hogen electrolyser H₂ at 1.35 MPa.
- Measurements corrected for error found during NPL calibration.
- Equivalent water vapour amount fraction values < 1 μmol mol⁻¹
- Fluctuations barely noticeable in slow responding Instrument F results compared to other instruments.
- Demonstrates the gas measured from the electrolyser met the specified purity of < 1 μmol mol⁻¹



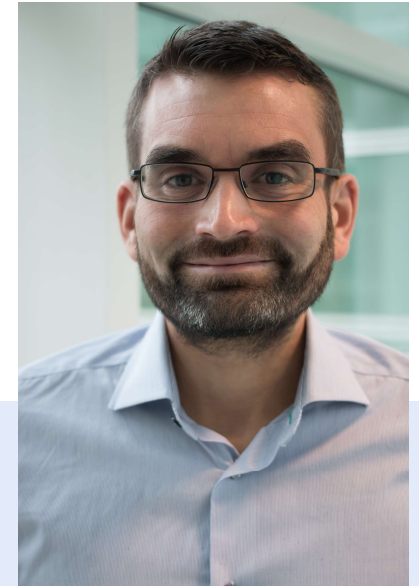
Task 1.3: Trials of rapid response analysis of key contaminants of hydrogen from electrolysis

- Additional NPL electrolyser measurements made as part of **Metrology for Hydrogen Vehicles 2** EMPIR project running in parallel to MefHySto with instruments calibrated in MefHySto.
- Measurements made at a Hydrogen refuelling station of hydrogen in the buffer tank at nominally 2 MPa.
- Instrument response time difference demonstrated during surge after 13:00.
- Reasonable agreement in measured value when errors found during NPL calibration corrected for and reference stable.



Work to be completed by project end

- CEA to perform testing of hydrogen quality produced by electrolyzers using water vapour spectrometer validated by PTB and an oxygen analyser loaned by collaborator.
- Testing of loan hygrometers in hydrogen / methane blends (80 % / 20 % , 50 % and 50 % WP5)
- WP1 Reports to be published:
- **D1**: 'Report on the development of new metrology for the measurement of key impurities in hydrogen (including water vapour and oxygen) produced from PEM water electrolyzers, with fast response times of a few or tens of seconds'.
- **D2**: 'Report on the testing of online gas analyser instruments for measuring key impurities (including water vapour and oxygen) in hydrogen from electrolysis in situ and during rapidly imposed transient use periods (0–100 %, 200 % peak)'.



Thank you! Questions?

Paul Carroll, (National Physical Laboratory –NPL, London, UK)
paul.carroll@npl.co.uk



The EMPIR initiative is co-funded by the European Union's Horizon 2020 research and innovation programme and the EMPIR Participating States



Single cell PEMFC testing with impure gases

MefHySto workshop, Berlin, 3 – 5 Jul 2023

Jonathan Goh, Graham Smith (NPL)

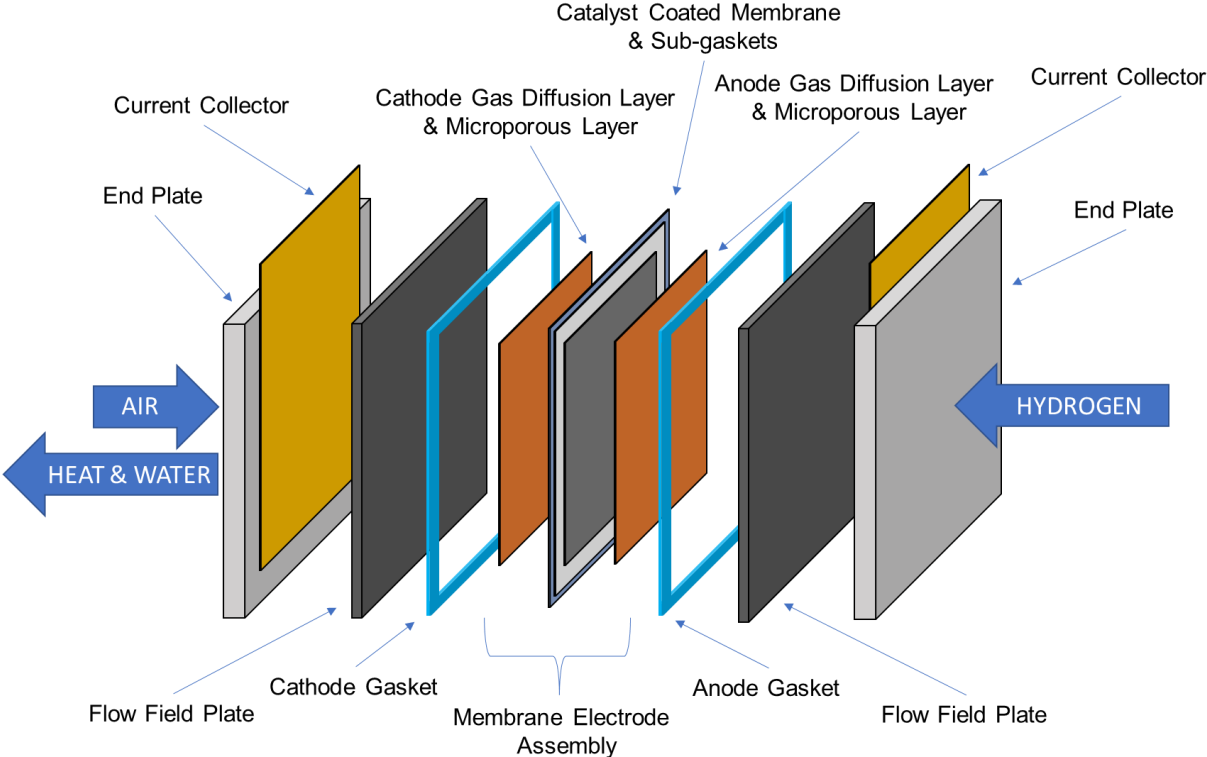
- Background
- Impurity Definitions & Impact
- Electrochemical Characterisation with Impure Gases



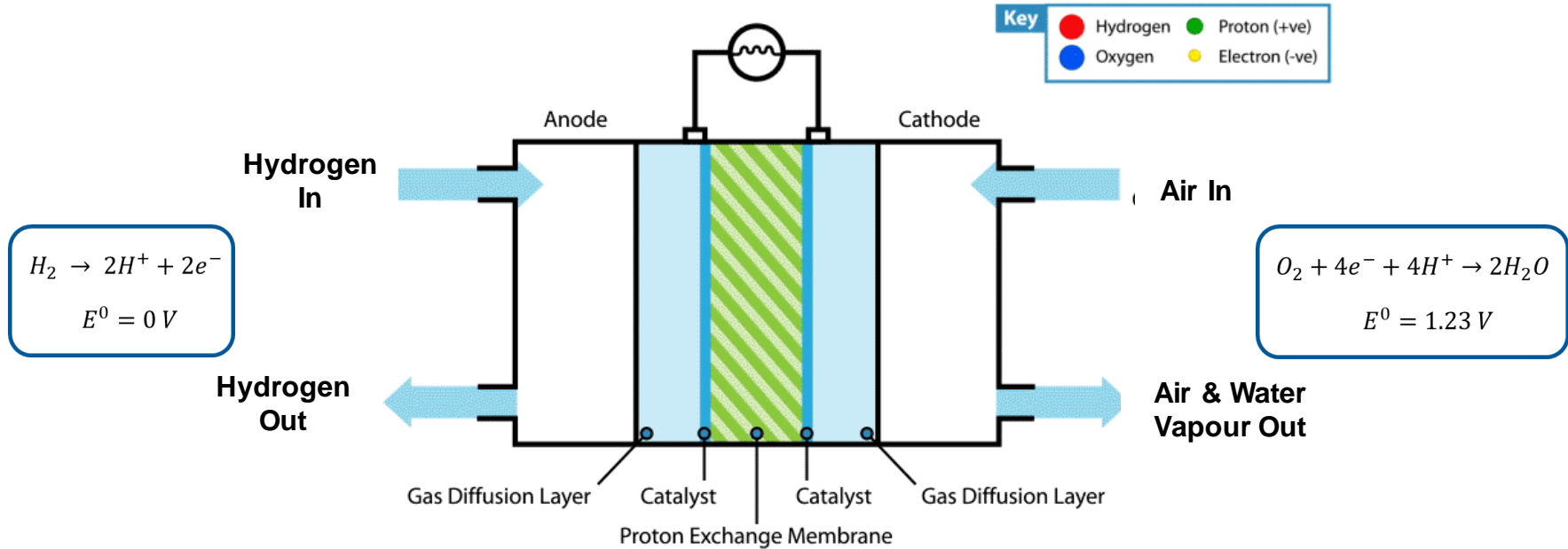
Background

Hydrogen & Fuel Cells

General components with a single cell PEMFC



Polymer electrolyte membrane fuel cell (PEMFC)





Impurity Definitions & Impact

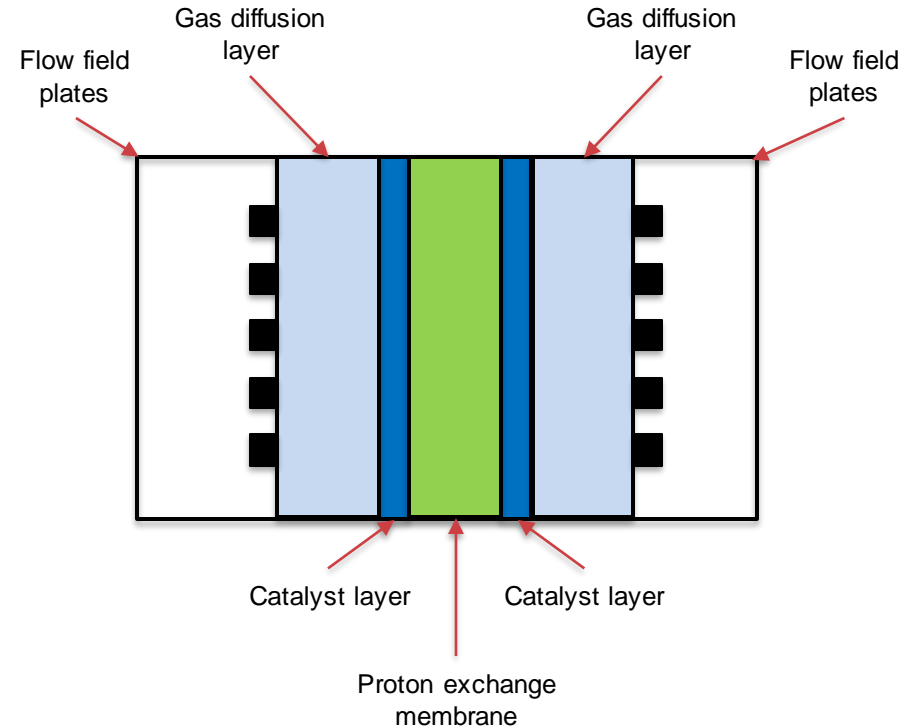
Standards, Scope & Impact

Hydrogen & Air quality

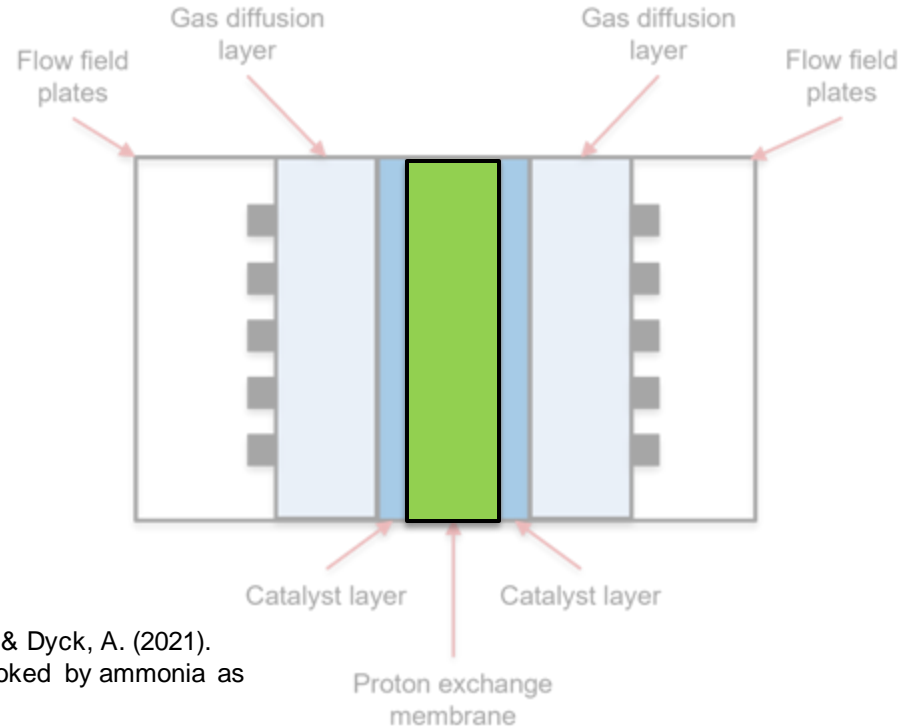
- **ISO 14687:2019(D)** – hydrogen quality for vehicular applications
 - Contaminant origins from hydrocarbon cracking/gasification
 - *Very little reported about the effect of complex mixtures on fuel cells*
- **Challenging to define standard for air quality** – type and concentration of contaminant dependent on area
 - Urban – SO_x , NO_x , particulate matter
 - Farm – NH_3
 - High altitude – low O_2 concentration

| Composition | Unit | ISO 14687:2019 (D) |
|-----------------------|--------------------------|--------------------|
| <i>Hydrogen</i> | <i>%</i> | <i>99.97</i> |
| Water | $\mu\text{mol mol}^{-1}$ | 5 |
| NMHC | $\mu\text{mol mol}^{-1}$ | 2 |
| Methane | $\mu\text{mol mol}^{-1}$ | 100 |
| Oxygen | $\mu\text{mol mol}^{-1}$ | 5 |
| Helium | $\mu\text{mol mol}^{-1}$ | 300 |
| Nitrogen | $\mu\text{mol mol}^{-1}$ | 300 |
| Argon | $\mu\text{mol mol}^{-1}$ | 300 |
| Carbon dioxide | $\mu\text{mol mol}^{-1}$ | 2 |
| Carbon monoxide | $\mu\text{mol mol}^{-1}$ | 0.2 |
| Sulfur compounds | $\mu\text{mol mol}^{-1}$ | 0.004 |
| Formaldehyde | $\mu\text{mol mol}^{-1}$ | 0.2 |
| Formic acid | $\mu\text{mol mol}^{-1}$ | 0.2 |
| Ammonia | $\mu\text{mol mol}^{-1}$ | 0.1 |
| Halogenated compounds | $\mu\text{mol mol}^{-1}$ | 0.05 |
| Particulates | mg/kg | 1 |

| Composition | Unit | ISO 14687:2019 (D) |
|-----------------------------|--------------------------|--------------------|
| <i>Hydrogen</i> | % | <i>99.97</i> |
| Water | $\mu\text{mol mol}^{-1}$ | 5 |
| NMHC (C1 eq.) | $\mu\text{mol mol}^{-1}$ | 2 |
| Methane | $\mu\text{mol mol}^{-1}$ | 100 |
| Oxygen | $\mu\text{mol mol}^{-1}$ | 5 |
| Helium | $\mu\text{mol mol}^{-1}$ | 300 |
| Nitrogen | $\mu\text{mol mol}^{-1}$ | 300 |
| Argon | $\mu\text{mol mol}^{-1}$ | 300 |
| Carbon dioxide | $\mu\text{mol mol}^{-1}$ | 2 |
| Carbon monoxide | $\mu\text{mol mol}^{-1}$ | 0.2 |
| Sulfur compounds (S1 basis) | $\mu\text{mol mol}^{-1}$ | 0.004 |
| Formaldehyde | $\mu\text{mol mol}^{-1}$ | 0.2 |
| Formic acid | $\mu\text{mol mol}^{-1}$ | 0.2 |
| Ammonia | $\mu\text{mol mol}^{-1}$ | 0.1 |
| Halogenated compounds | $\mu\text{mol mol}^{-1}$ | 0.05 |
| Particulates | mg/kg | 1 |

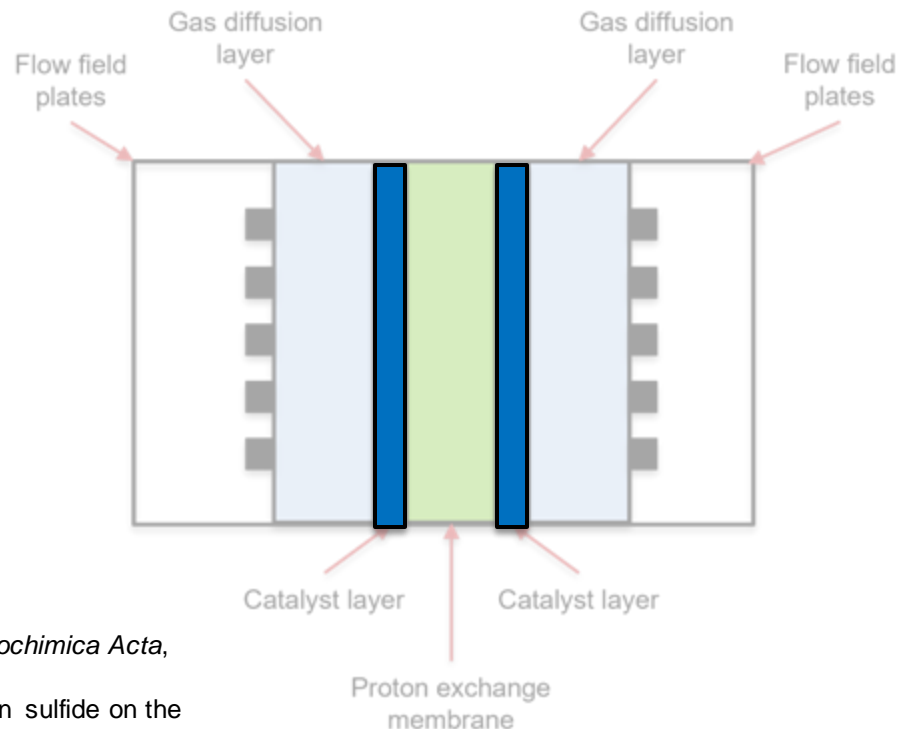


- **NH₃** contaminates membrane/ionomer, even at 1 ppm
- **Halogens** cause membrane dissolution
 - NaCl reduces membrane ionic conductivity
- **Fe³⁺** contamination at 1 ppm occupies ion exchange sites on membrane (and active sites on catalyst layer)
 - Fe³⁺ → H₂O₂ → free radicals
 - Membrane deterioration



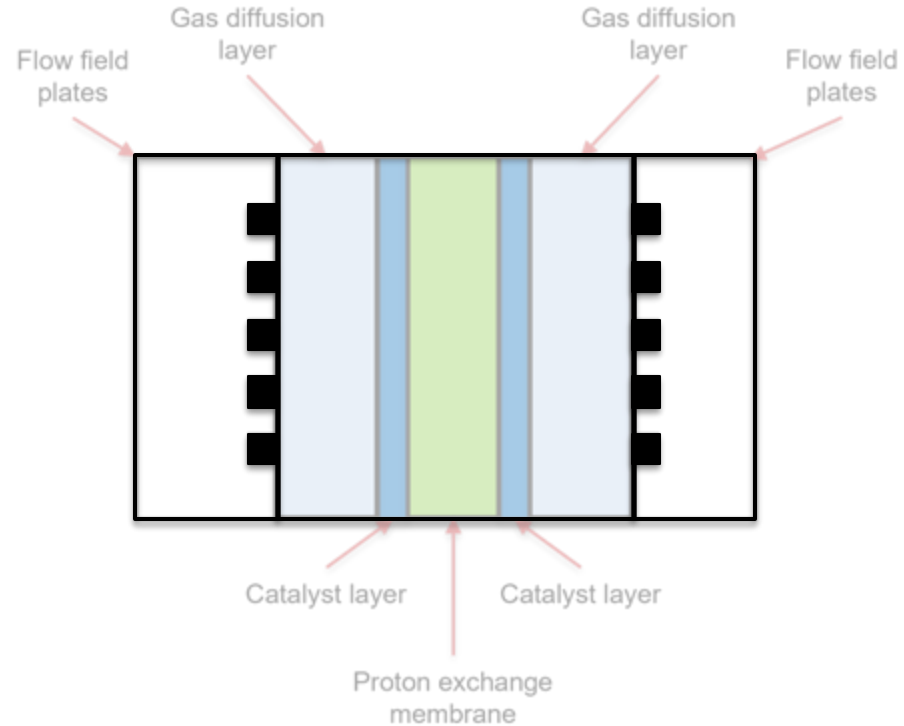
1. Schonvogel, D., Büsselmann, J., Schmies, H., Langnickel, H., Wagner, P., & Dyck, A. (2021). High temperature polymer electrolyte membrane fuel cell degradation provoked by ammonia as ambient air contaminant. *Journal of Power Sources*, 502(May), 229993. <https://doi.org/10.1016/j.jpowsour.2021.229993>

- CO binds with Pt active sites, reversibly
- H₂S severely poisons catalyst, irreversibly
- CO₂ could potentially convert to CO – not widely documented
- CH₂O₂ can cross PEM and contaminate cathode; at 100 ppm may cause coarsening or dissolution of Pt



1. St-Pierre, J. (2010). PEMFC contaminant tolerance limit—CO in H₂. *Electrochimica Acta*, 55(13), 4208–4211. <https://doi.org/10.1016/J.ELECTACTA.2010.02.061>
2. Lopes, T., Paganin, V. A., & Gonzalez, E. R. (2011). The effects of hydrogen sulfide on the polymer electrolyte membrane fuel cell anode catalyst: H₂S-Pt/C interaction products. *Journal of Power Sources*, 196(15), 6256–6263. <https://doi.org/10.1016/j.jpowsour.2011.04.017>

- CH_4 , CO_2 , He, Ar, N_2 etc. dilute hydrogen
 - Effect is more severe with a recirculation loop
 - CO_2 crossover from cathode to anode can lead to high concentrations at the anode

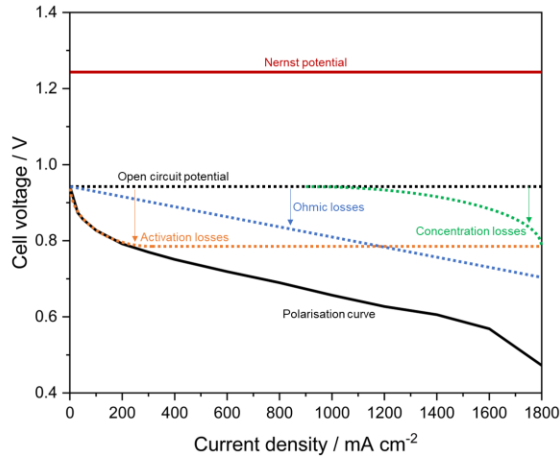


- **Tetrachloroethylene** and **hydrogen chloride** cause rapid cell degradation even at $0.05 \mu\text{mol mol}^{-1}$
 - Chloride compounds may precipitate and block mass flow
- **Particulate matter** can clog filters and affect valves
 - Deposition of particles on catalyst layer can cause membrane rupture → short circuits
 - Fe containing particles can cause catalyst/membrane degradation
- **Hydrocarbons (except methane)** cause varied effects
 - Shorter HCs may act only as diluents
 - Longer HCs may alter wettability of components, poison catalyst or block mass flow
- **Oxygen** degrades fuel cell
 - Explosion hazard within flammability limit 4 – 94 % concentration (hydrogen in oxygen)
 - May mitigate catalyst poisoning
- **Water** has no direct impact on fuel cell performance, but
 - May facilitate poisoning by ionic species
 - May alter thermodynamic properties of gases
 - May reduce hydrogen storage capacity a damage storage tanks

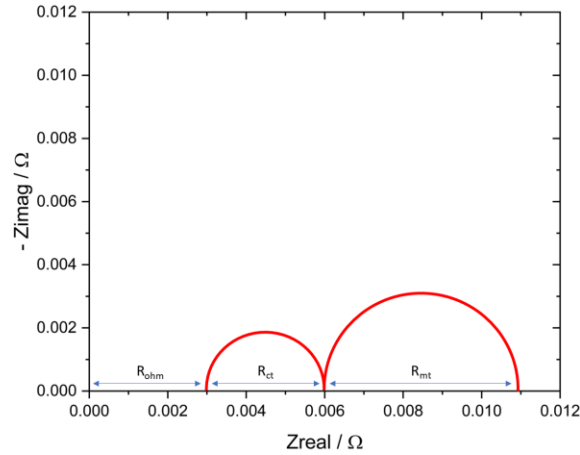


Electrochemical Characterisation

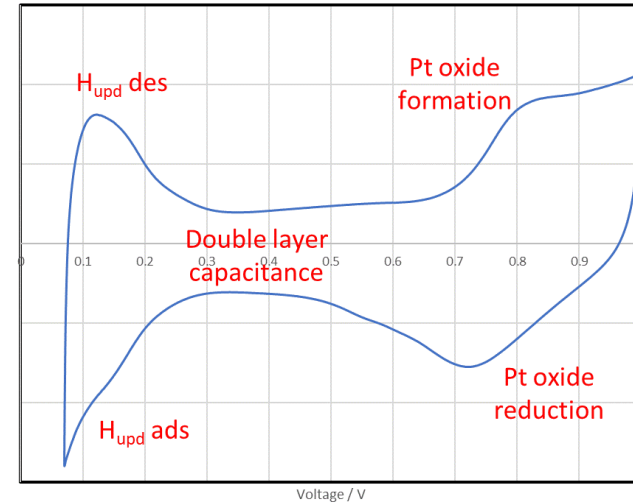
In situ & In operando methods



Polarisation curve



EIS
(Nyquist plot)



Cyclic
voltammogram



Thank you!

jonathan.goh@npl.co.uk



The EMPIR initiative is co-funded by the European Union's Horizon 2020 research and innovation programme and the EMPIR Participating States